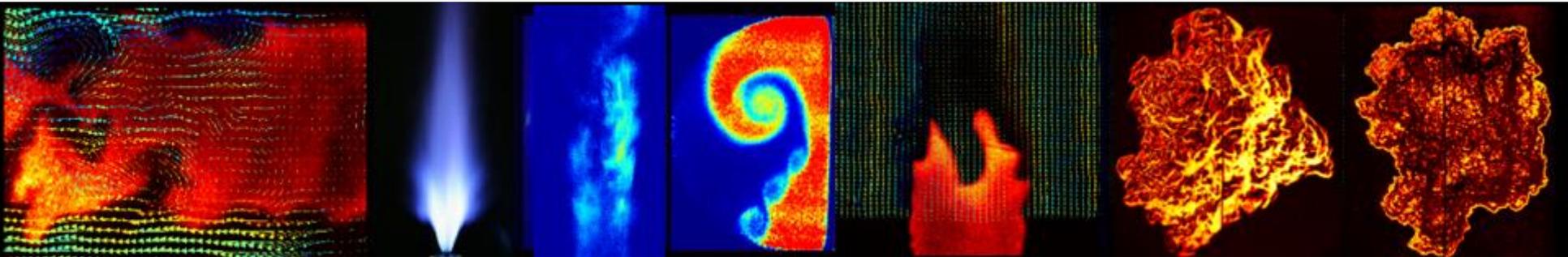




# Blowoff Dynamics and its Measurements



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# Bluff body and swirl stabilized flames

Bluff body and swirl stabilized flames are ubiquitous in propulsion and land based power generation systems

Aerospace propulsion: Ramjet and turbojet afterburners and even scramjets, industrial combustion systems, boilers and heat recovery steam generators use bluff body flame stabilizations.

Most gas turbine combustors: swirl flames.

Basic motivation behind use of a bluff body or swirl: To create a local low velocity recirculating flow region that continuously ignites the fresh mixture and sustains reactions in an otherwise high speed flow.



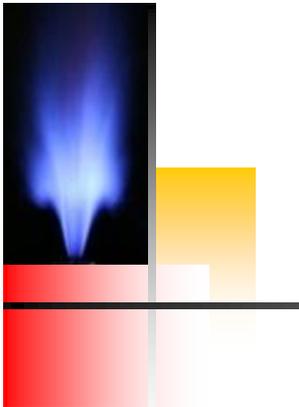
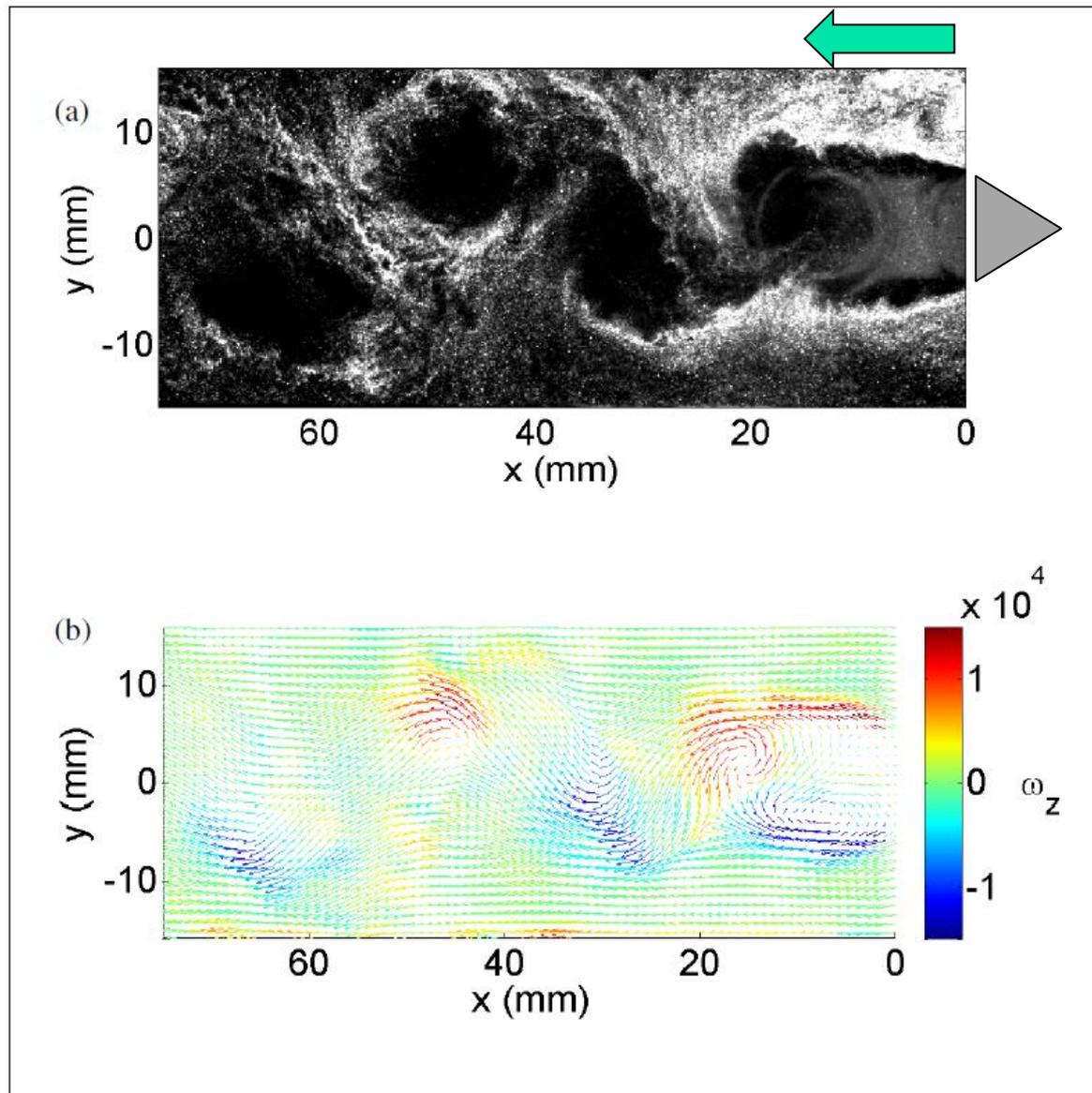
## Blowoff

- Only within a certain range of conditions governed by fluid mechanics and chemical kinetics a flame can be stabilized by a bluff body.
- Even though it is trivial enough to assume correctly that leaning out the fuel concentration will lead to flame extinction and blowoff, its exact mechanism remained unsolved with works presented in *over 150 articles over the last five decades*.

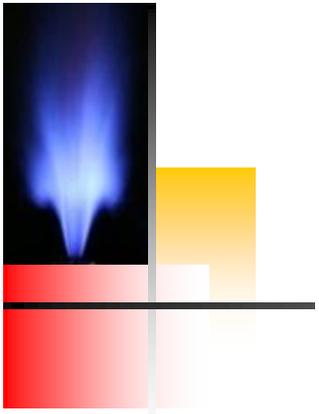
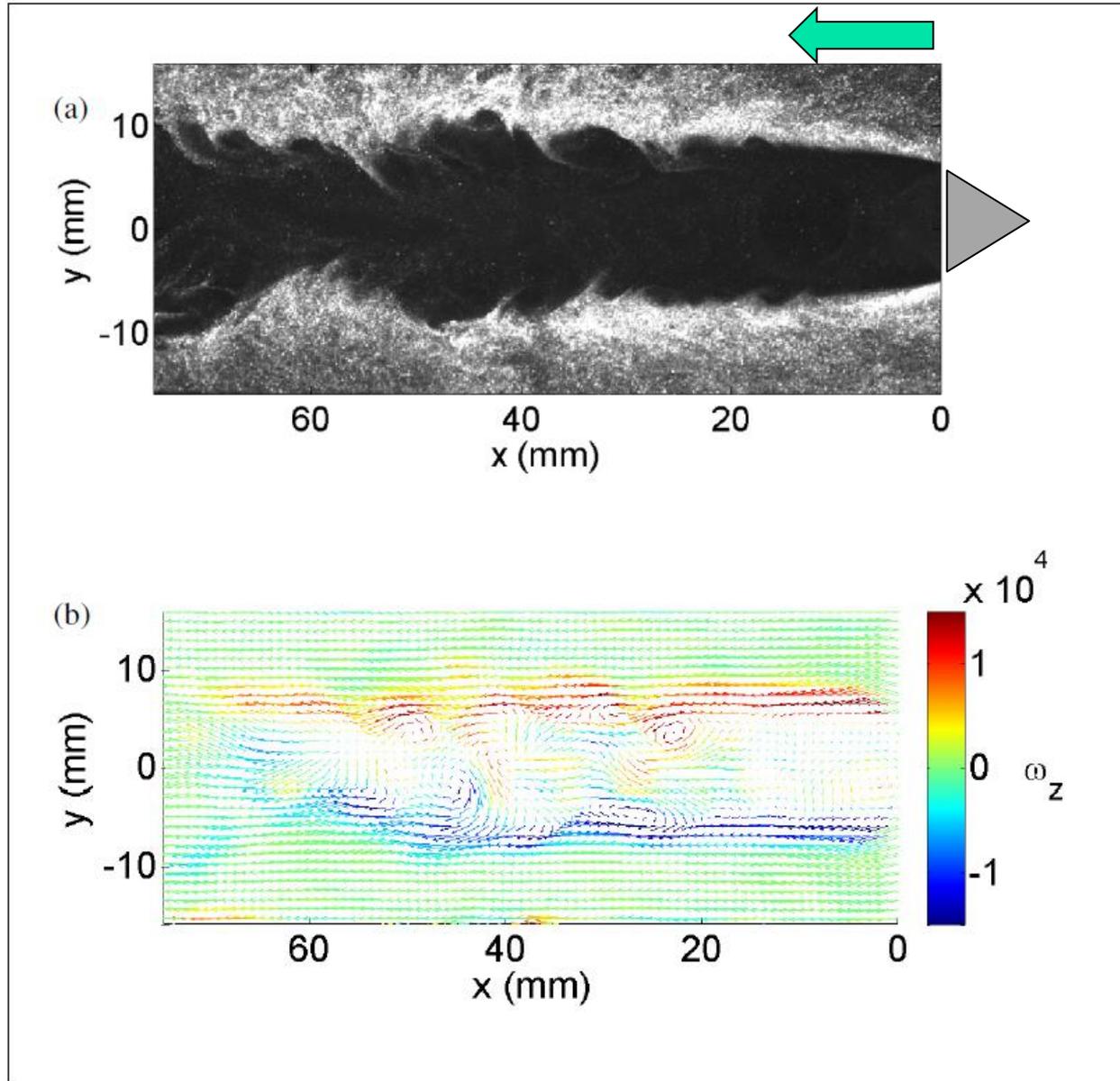


Flame blowoff in the SR-71 during a high-acceleration turn, Campbell and Chambers

## Characteristics of flows separated by bluff bodies: Non-reacting flows



# Characteristics of flows separated by bluff bodies: Reacting flows





## Effects of exothermicity

Results indicate substantially reduced turbulence intensities and vorticity magnitudes in combustions flows relative to the non-reacting flow for e.g. by Soteriou, Ghoniem (1994).

Fureby and Lofstrom (1994): vorticity field strength was much weaker and “less structured” (1994) in the presence of combustion.

Fuji and Eguchi (1981) and Bill and Tarabanis (1986) noted that turbulence levels in the reacting flow were much lower than the non-reacting case, particularly in the vicinity of the recirculation zone boundary.



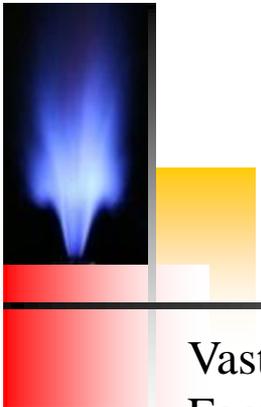
## The Vorticity Transport Equation

$$\frac{D\vec{\omega}}{Dt} = \underbrace{(\vec{\omega} \cdot \vec{\nabla})\vec{V}}_{\text{Vortex Stretching}} - \underbrace{\vec{\omega}(\vec{\nabla} \cdot \vec{V})}_{\text{Gas Expansion}} - \underbrace{\frac{\vec{\nabla} p \times \vec{\nabla} \rho}{\rho}}_{\substack{\text{Baroclinic} \\ \text{Vorticity} \\ \text{Production}}} + \underbrace{\vec{\nabla} \times \frac{\vec{\nabla} \cdot \vec{S}}{\rho}}_{\text{Viscous Diffusion}}$$

The kinematic gas viscosity, in term 4 rapidly increases through the flame, due to its larger temperature sensitivity. This substantially enhances the rate of diffusion and damping of vorticity, an effect emphasized by Coats (1996)

Term 3, i.e. the Baroclinic vorticity production, originates from the pressure and density gradient mismatch.

Term 2, i.e. dilatation also acts as a vorticity sink



# Outline

Vast topic studied by combustion researchers for decades  
Focus of premixed and to some extent on partially premixed flames.

## 1. Blowoff in Bluff Body Stabilized Premixed Flames

- Asses the developments in the field characterized by advent and implementation of sophisticated measurements.
- Nair and Lieuwen (2005-9s) used mie scattering and optical emission.
- Chaudhuri, Cetegen et al (2008-10s) used chemiluminescence imaging and simultaneous PIV PLIF.
- Kariuki, Mastorakos et al (2011-13s) used high speed PIV-PLIF.

## 2. Forced Blowoff, Vitiated (as in an afterburner) blowoff

## 3. Blowoff in Swirl Stabilized Flames

- Murgunandam, Seitzman (2005s) used chemiluminescence imaging; optical fiber coupled probes for control of blowoff
- Stoehr, Meier (2011s) used high speed PIV-PLIF.

## 4. Related Insights:



# Near Blowoff Dynamics in Bluff Body Stabilized Flames

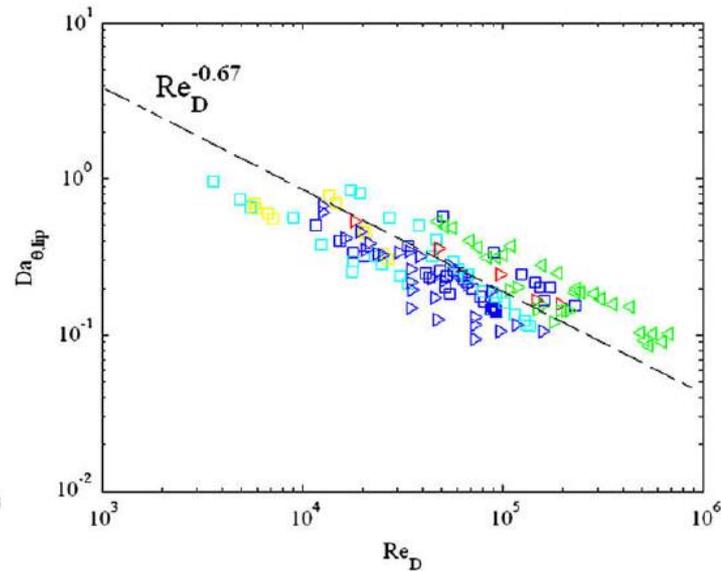
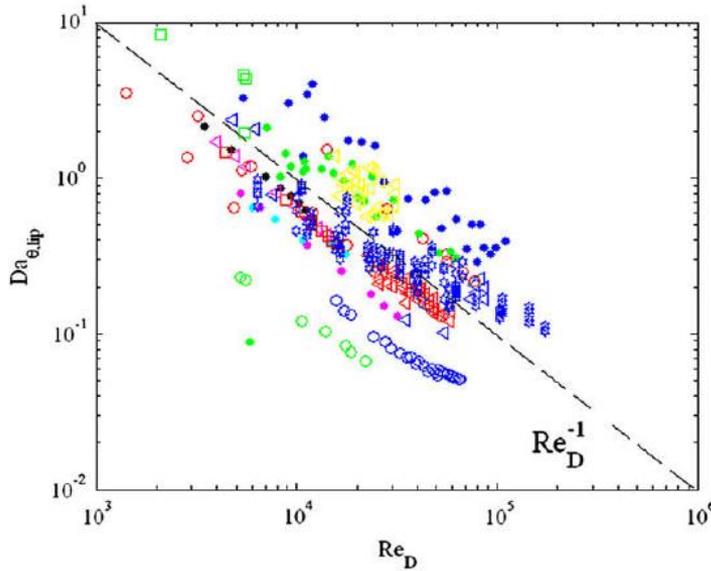
- Many researchers observed that near blowoff flames are highly unsteady and unstable (Zukoski (1958), Williams (1966) H.M. Nicholson (1948))
- Nicholson and Field (1948) described large scale pulsations in rich bluff body flames as they were blowing off.
- Observations of large scale, sinuous oscillations of a flame near blowoff were presented by Thurston (1958).
- Hertzberg et al. (1991) measured velocity fluctuations in a bluff body wake, indicating a growing amplitude of a relatively narrowband oscillation as blowoff was approached that they attributed to vortex shedding.
- A number of more recent studies by Nair and Lieuwen (2007), Kiel et al. (2007) and Erickson et al. have also noted these dynamics (2007).



## Early views on blowoff

- Longwell (1953) suggested: blowoff due to imbalance in rate of entrainment of reactants (a PSR RZ)
- Insufficient heat supply by RZ to fresh gases (Williams GC, Hottel H. et al. 1951)
- Insufficient contact time of the fresh mixture in the shear layer with the burnt product in RZ. (Zukoski 1954)
- Extinction of a strained flamelet (Yamaguchi 1985)
- But these studies did not connect the early stages of blowoff dynamics with the final blowoff event as complete mechanism was lacking.

# Blowoff Correlation



Correlation of two-dimensional (left) and axisymmetric (right) bluff body data sets showing  $Da_{e, lip}$  at blowoff as a function of  $Re_D$  utilizing  $T_{PSR}$  as the chemical time. (Shanbhogue 2009)

$$Da = bRe_D^a \Rightarrow \log(Da) = a \log(Re_D) + b$$

Summary of data used for data compilation reported (italicized and non-italicized text under "Bluff body type" denotes axisymmetric and nominally two-dimensional bluff body, respectively).

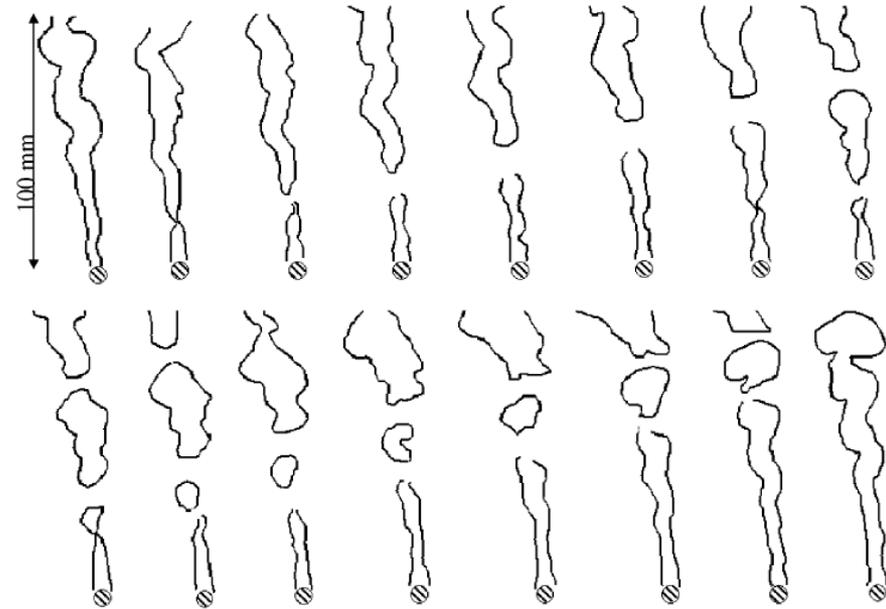
| Reference                 | Symbol                      | Symbol color       | Ref. year | U (m/s) | $Re_D \times 1000$ | P (atm)  | Inlet temp(K) | Fuel       | Bluff body type        |
|---------------------------|-----------------------------|--------------------|-----------|---------|--------------------|----------|---------------|------------|------------------------|
| DeZubay [77]              | $\square, \square, \square$ | Blue, cyan, yellow | 1950      | 30-98   | 60-200             | 0.2-1    | 305           | Propane    | <i>Circular disk</i>   |
| Plee and Mellor [80]      | $\triangleright$            | Blue               | 1979      | 10-100  | 12-148             | 0.9      | 300           | Propane    | <i>Closed v-gutter</i> |
| C.R. King [140]           | $\triangleleft$             | Blue               | 1957      | 11-200  | 13-230             | 0.85     | 680           | JP-4       | <i>Open v-gutter</i>   |
| Longwell et al. [141]     | $\triangleleft$             | Green              | 1948      | 72-254  | 223-782            | 1        | 422           | Pentane    | <i>Open v-gutter</i>   |
| Zukoski [16]              | $\circ$                     | Blue               | 1954      | 47-194  | 15-62              | 1        | 339           | Gasoline   | Cylinder               |
| G. C. Williams [142]      | $\bullet, \circ$            | Blue, red          | 1949      | 8-64    | 11-90              | 1        | 300           | Propane    | Cylindrical rod        |
| Sanquer et al. [143]      | $\square$                   | Green              | 1998      | 2.9-7.6 | 2-6                | 1        | 280           | Propane    | Triangle, rectangle    |
| Yamaguchi et al. [68]     | $\bullet$                   | Green              | 1985      | 8.5-39  | 12-52              | 1        | 295           | Propane    | Cylinder               |
| Hottel et al. [78]        | $\triangleleft$             | Red                | 1962      | 40-82   | 12-63              | 0.4,0.6  | 394           | Propane    | <i>Open v-gutter</i>   |
| Loblich [144]             | $\bullet$                   | Red                | 1962      | 9-80    | 4-36               | 1        | 293           | Propane    | Cylinder               |
| Fetting [145]             | $\bullet$                   | Cyan               | 1958      | 10-100  | 4-26.5             | 1        | 300           | Propane    | Cylinder               |
| Filippi [146]             | $\bullet$                   | Magenta            | 1960      | 10-100  | 4-26.5             | 1        | 300           | Propane    | Cylinder               |
| Scurlock [147]            | $\bullet$                   | Yellow             | 1948      | 20-95   | 18-64              | 1        | 300           | Propane    | Cylinder               |
| von Gerichten [92]        | $\circ$                     | Green              | 1954      | 30-130  | 4.5-20             | 1        | 339           | Gasoline   | Cylinder               |
| Ballal and Lefebvre [148] | $\triangleright$            | Red                | 1979      | 10-100  | 17-183             | 0.89     | 300           | Propane    | <i>Closed cone</i>     |
| Hanna et al. [149]        | $\triangleright$            | Green              | 1989      | 60-180  | 150-301            | 1        | 500           | Diesel oil | <i>Closed cone</i>     |
| Barrère and Mestre [95]   | $\bullet$                   | Black              | 1985      | 8-45    | 3-16               | 1        | 290           | Propane    | Cylinder               |
| Barrère and Mestre [95]   | $\triangleleft$             | Magenta            | 1954      | 9-45    | 4-16               | 1        | 290           | Propane    | <i>Open v-gutter</i>   |
| Barrère and Mestre [95]   | $\square$                   | Red                | 1954      | 10-45   | 5-16               | 1        | 290           | Propane    | Plate                  |
| Yang, Yen, and Tsai [97]  | $\triangleleft$             | Yellow             | 1994      | 14-27   | 15-31              | 0.99     | 298           | LPG        | <i>Open v-gutter</i>   |
| Potter and Wong [74]      | $\square$                   | Blue               | 1958      | 20-130  | 6.4-173            | 0.3-0.93 | 300           | Propane    | Cylinder               |

Shanbhogue et al (2009)

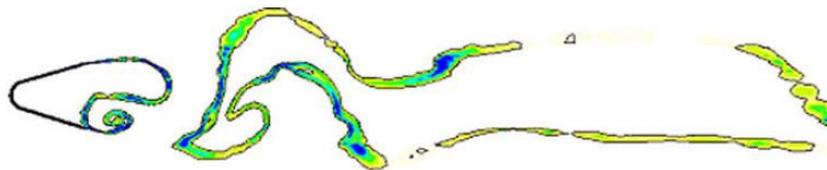
# Works at Georgia Tech: Two stages of blowoff

## Stage 1:

Initiation of flame hole, its convection downstream and healing. However the flame can persist indefinitely at this stage. This local extinction is hypothesized to be occurring at points where  $k_{\text{local}} > k_{\text{extinct}}$

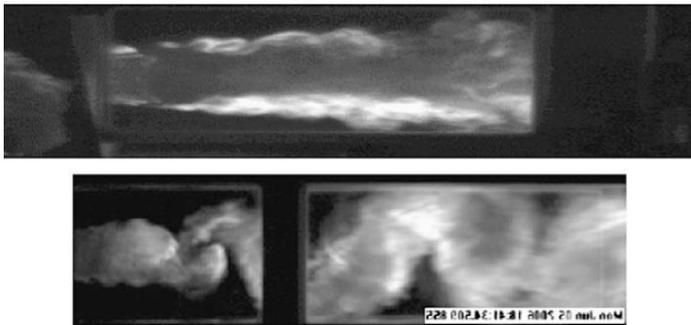


Sequence of flame images, 10 ms apart, taken during the first preblowoff stage at  $\phi = 0.65$ . Note presence of flame holes in the images (flow direction is from bottom to top). Nair and Lieuwen (2007)

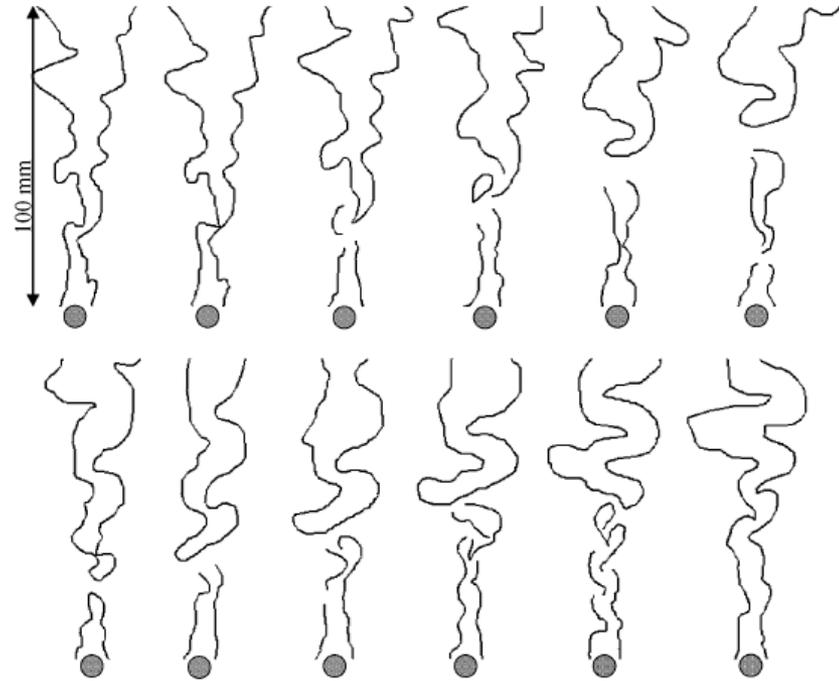


Computed reaction rate contours of a V-Gutter stabilized flame exhibiting localized extinction ( $Re_D = 56,000$ ,  $T_b/T_u = 2.9$ ) (Smith et al (2007))

**Stage 2:**  
Moments away from blowoff



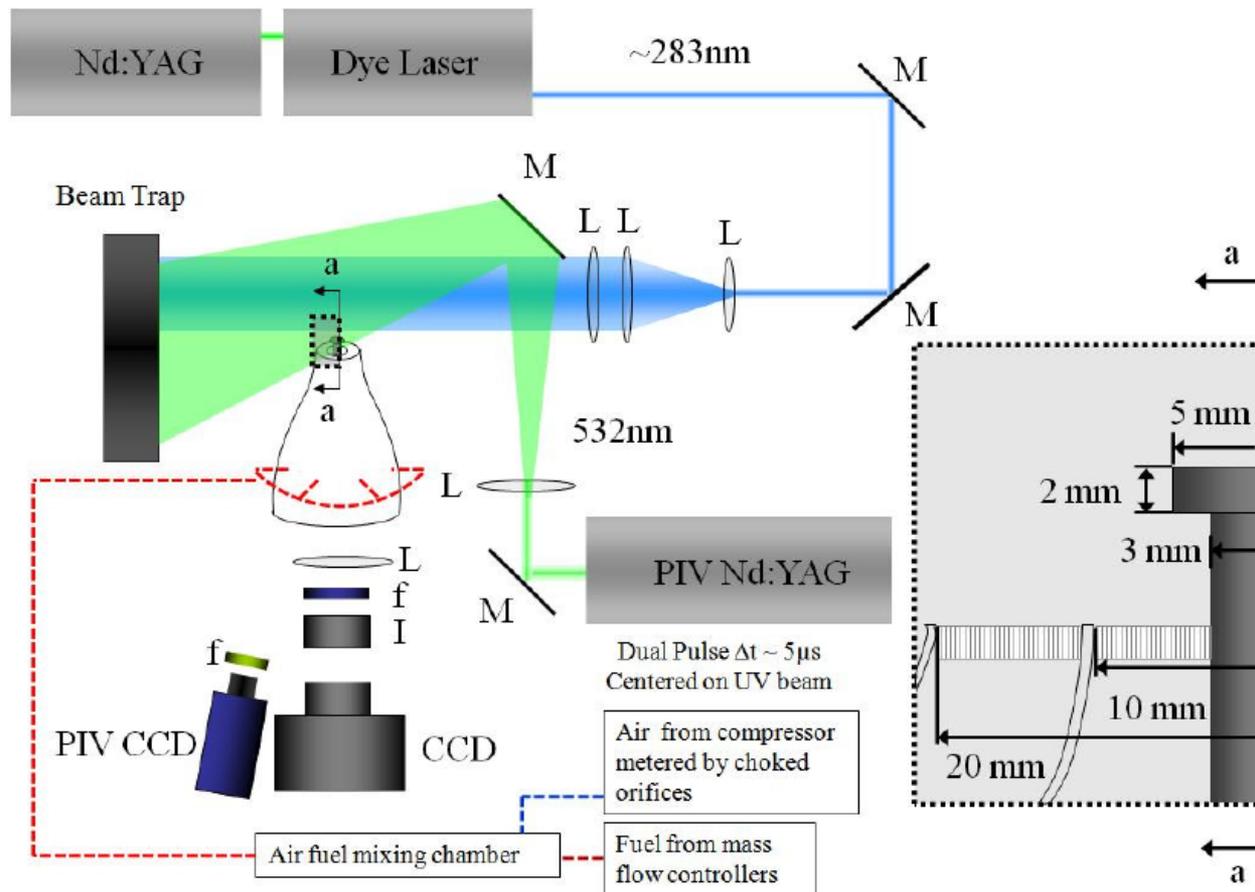
Measured high speed chemiluminescence images of V-gutter flames, at high equivalence ratio ( $Re_D = 30,000$ ,  $T_b/T_u = 5.9$ ) (top) & close to blowoff ( $Re_D = 35,000$ ,  $T_b/T_u = 3$ ) (below). Picture reproduced from Kiel et al (2007)



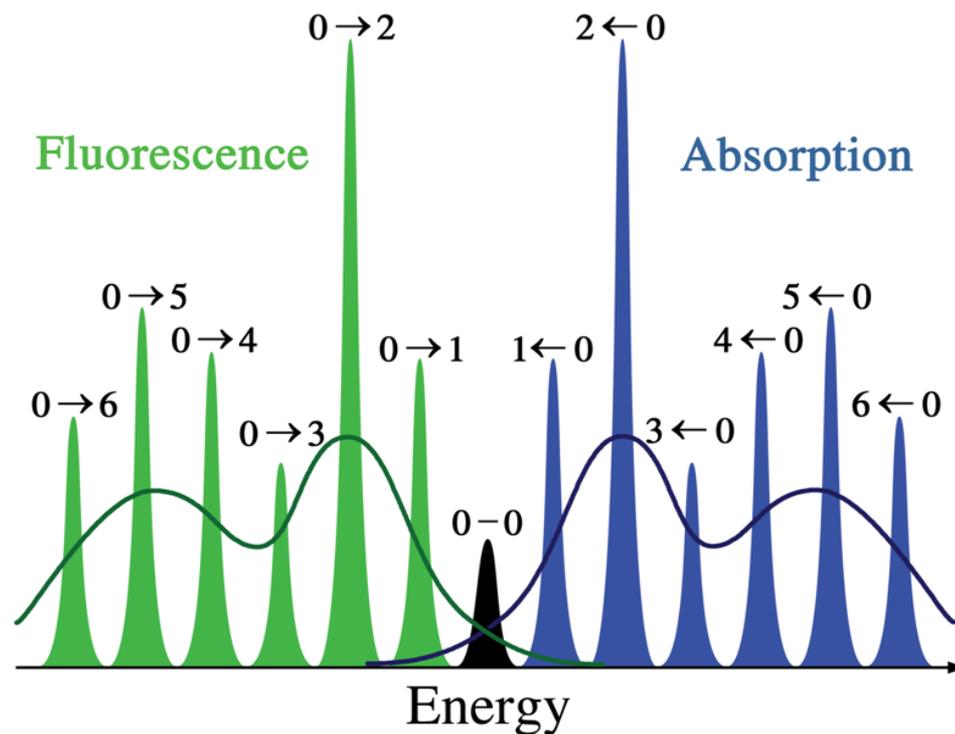
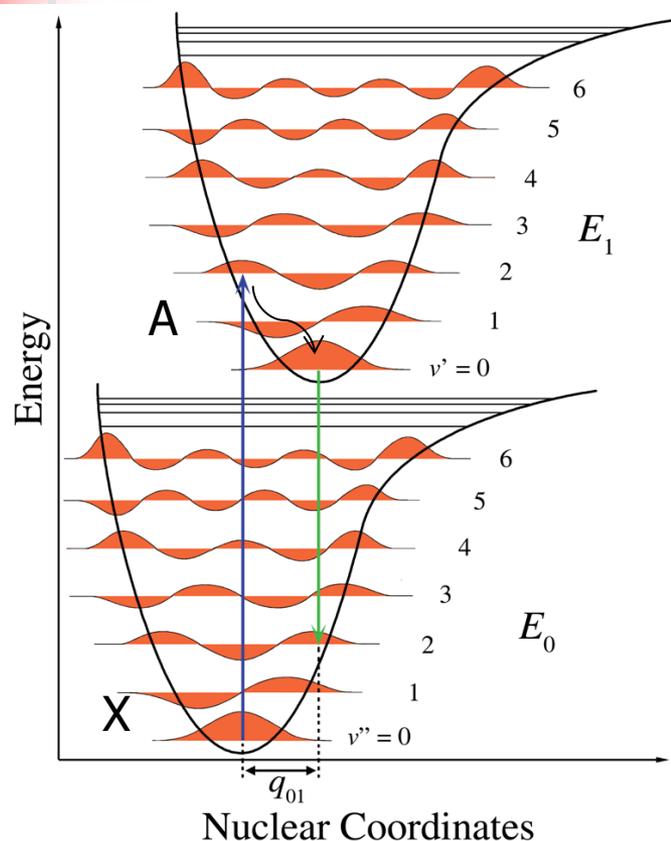
Sequence of flame images, 6 ms apart, taken during the second preblowoff stage at  $\phi = 0.6$  (flow direction is from bottom to top)  
Nair and Liewen (2007)

Return to asymmetry near blowoff

# Works at UConn with lean propane air flames



# Laser Induced Fluorescence



Fluorescence occurs at a low frequency than the incident radiation because the emissive transition occurs after some energy has been discarded into the surroundings.

# Single photon laser induced fluorescence species concentration detection: model

## Two level model:

$b_{12}$  and  $b_{21}$  :rate constants for absorption and stimulated emission and are related to the Einstein coefficients by

$$b = \frac{BI_\nu}{c}$$

$$\frac{dN_1}{dt} = \dot{N}_1 = -N_1 b_{12} + N_2 (b_{21} + A_{21} + Q_{21})$$

$$\frac{dN_2}{dt} = \dot{N}_2 = N_1 b_{12} - N_2 (b_{21} + A_{21} + Q_{21} + P + W_{2i})$$

$b, A, Q, P, W$  are termed rate constants

$A$  = Einstein A coefficient

$P$  = Predissociation rate constant

$W_{2i}$  = photoionization rate constant

**$Q$  = collisional quenching rate.**

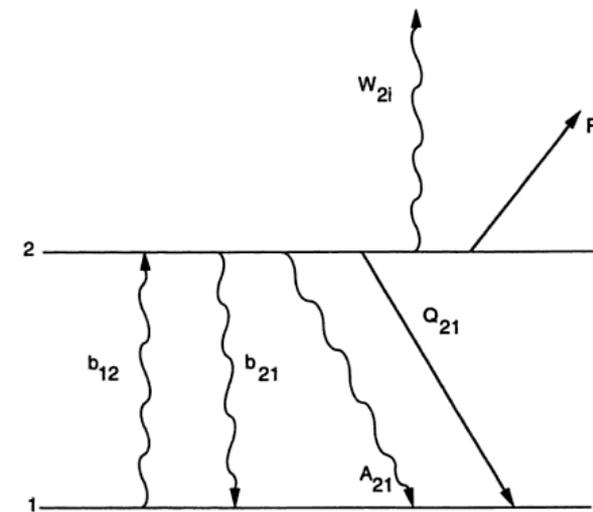


Fig 7. Simple two energy level diagram for LIF modelling. from [1]



... continued

Neglecting predissociation and photoionization we get

$$\frac{dN_1}{dt} + \frac{dN_2}{dt} = 0$$

$$\therefore N_1 + N_2 = N_1^0 = \text{cons.} = \text{species population prior to excitation}$$

The Fluorescence signal is proportional to  $N_2 A_{21}$  and hence we need to relate

$$N_2 \rightarrow N_1^0$$

**This is done by eliminating  $N_1$  from the  $N_2$  rate equation and integrating we get:**

$$N_2(t) = \frac{b_{12} N_1^0}{r} (1 - e^{-rt}) \quad \text{where } r = b_{12} + b_{21} + A_{21} + Q_{21} \\ \text{and } N_2(t=0) = 0$$



... continued

$$N_2(t) = \frac{b_{12}N_1^0}{r} \quad \text{at steady state}$$

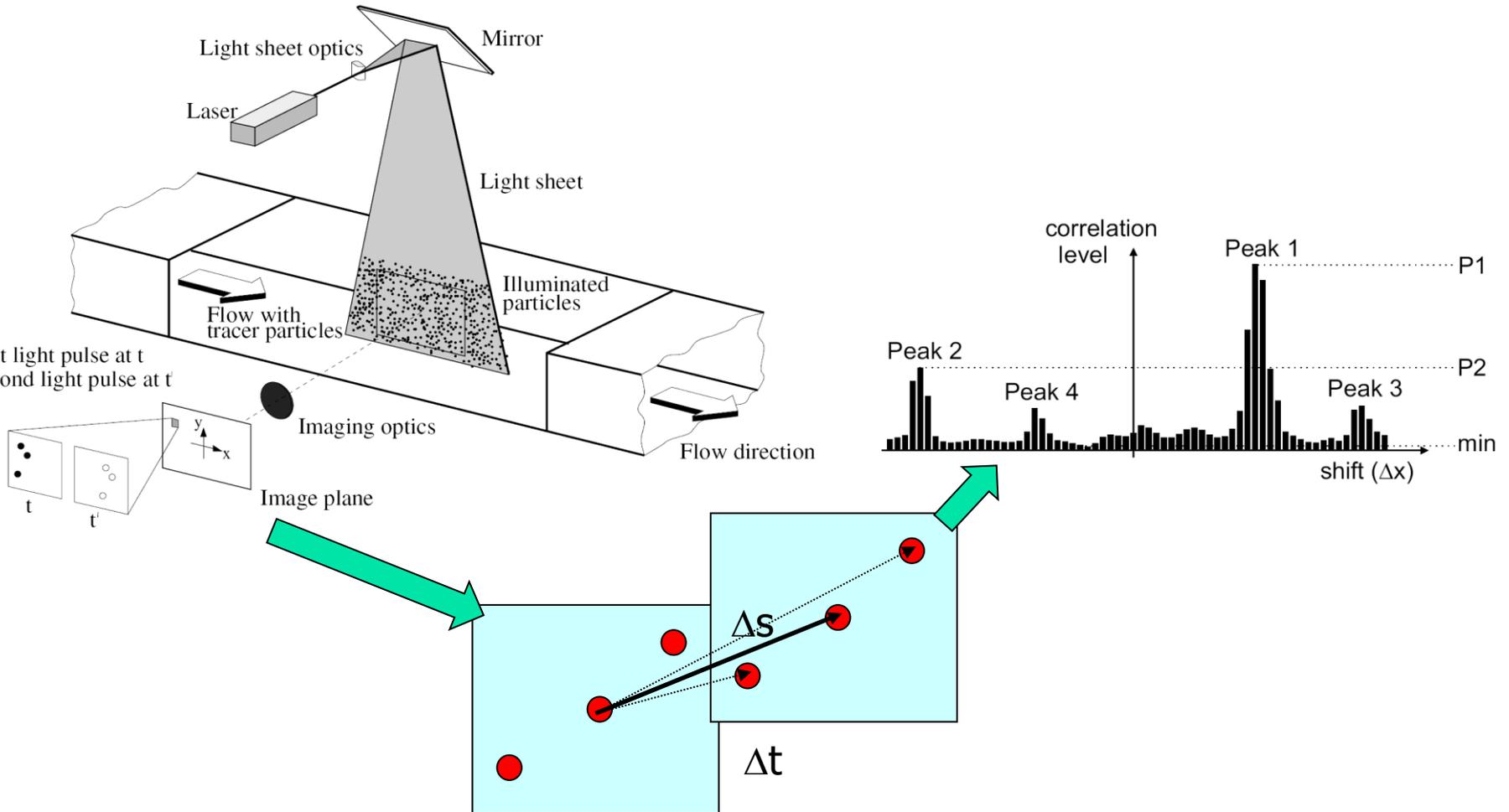
$$F = h\nu N_2 A_{21} \frac{\Omega}{4\pi} lA \sim N_1^0 \frac{B_{12}}{B_{12} + B_{21}} \frac{A_{21}}{1 + \frac{I_{sat}^\nu}{I_\nu}}$$

$$I_{sat}^\nu = \frac{(A_{21} + Q_{21})c}{B_{12} + B_{21}} \quad \text{Saturation spectral intensity}$$

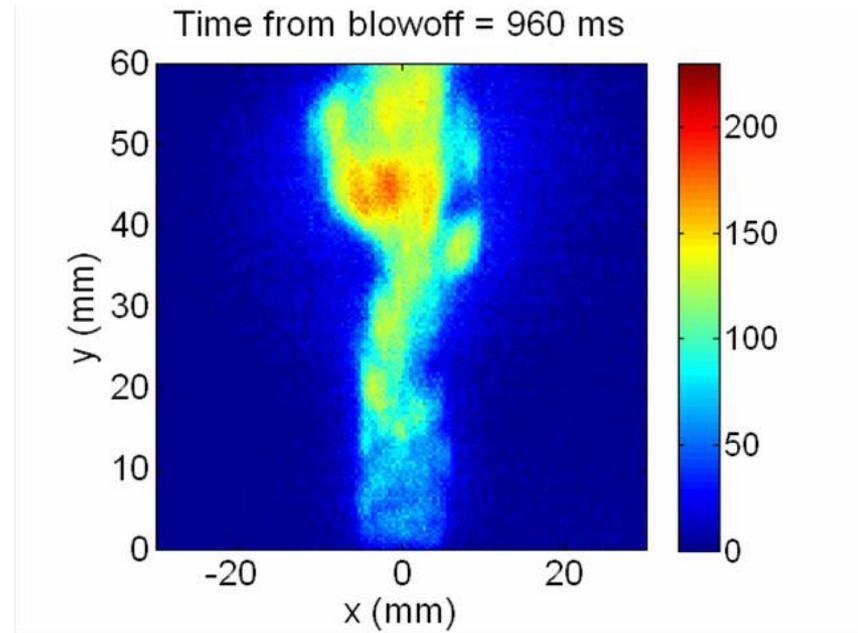
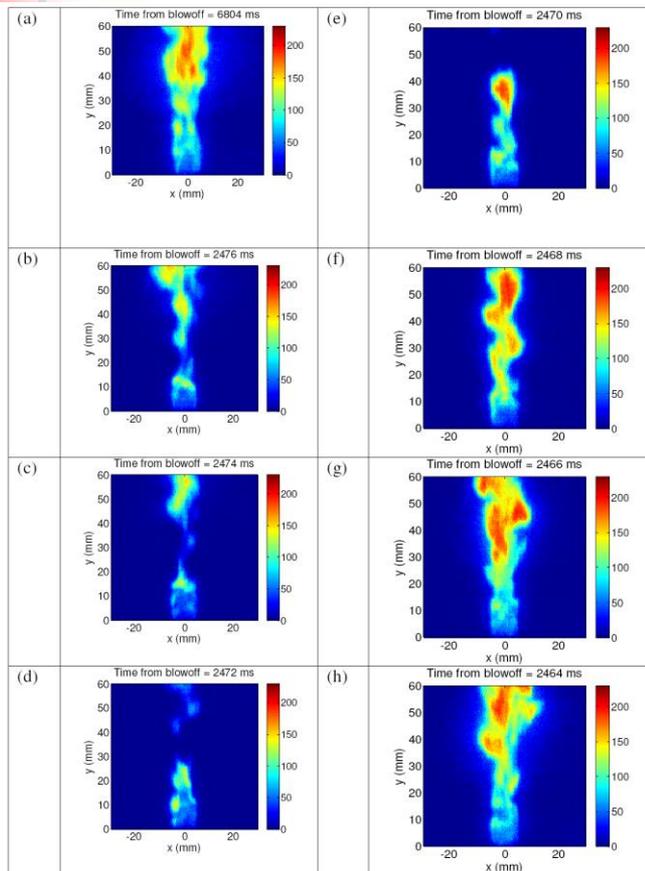
$$F \sim N_1^0 \frac{B_{12}I_\nu}{B_{12} + B_{21}} \frac{A_{21}}{A_{21} + Q_{21}} \dots \text{for } I_\nu \ll I_{sat}^\nu$$

$$F \sim N_1^0 \frac{B_{12}}{B_{12} + B_{21}} A_{21} \dots \text{for } I_\nu \gg I_{sat}^\nu$$

# Particle Image Velocimetry



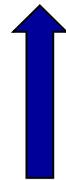
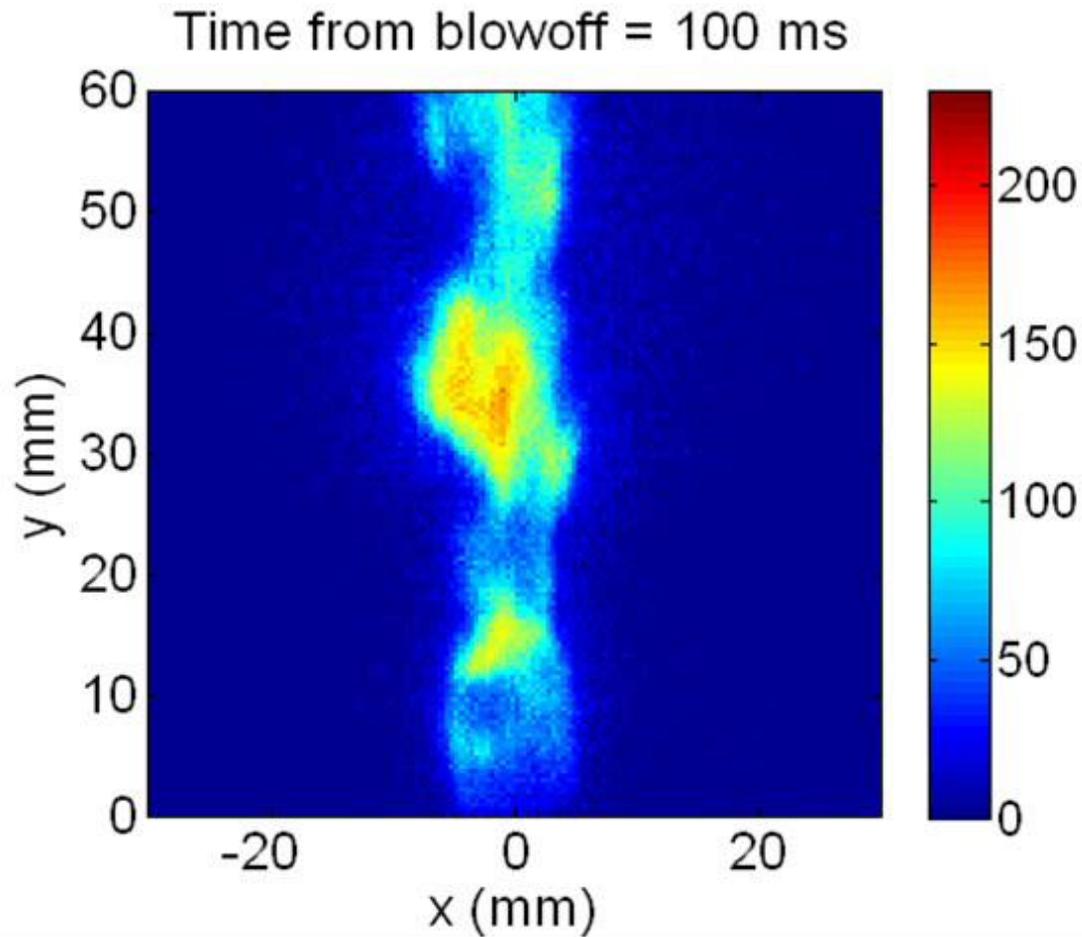
# Time resolved chemiluminescence imaging



Extinction and Reignition

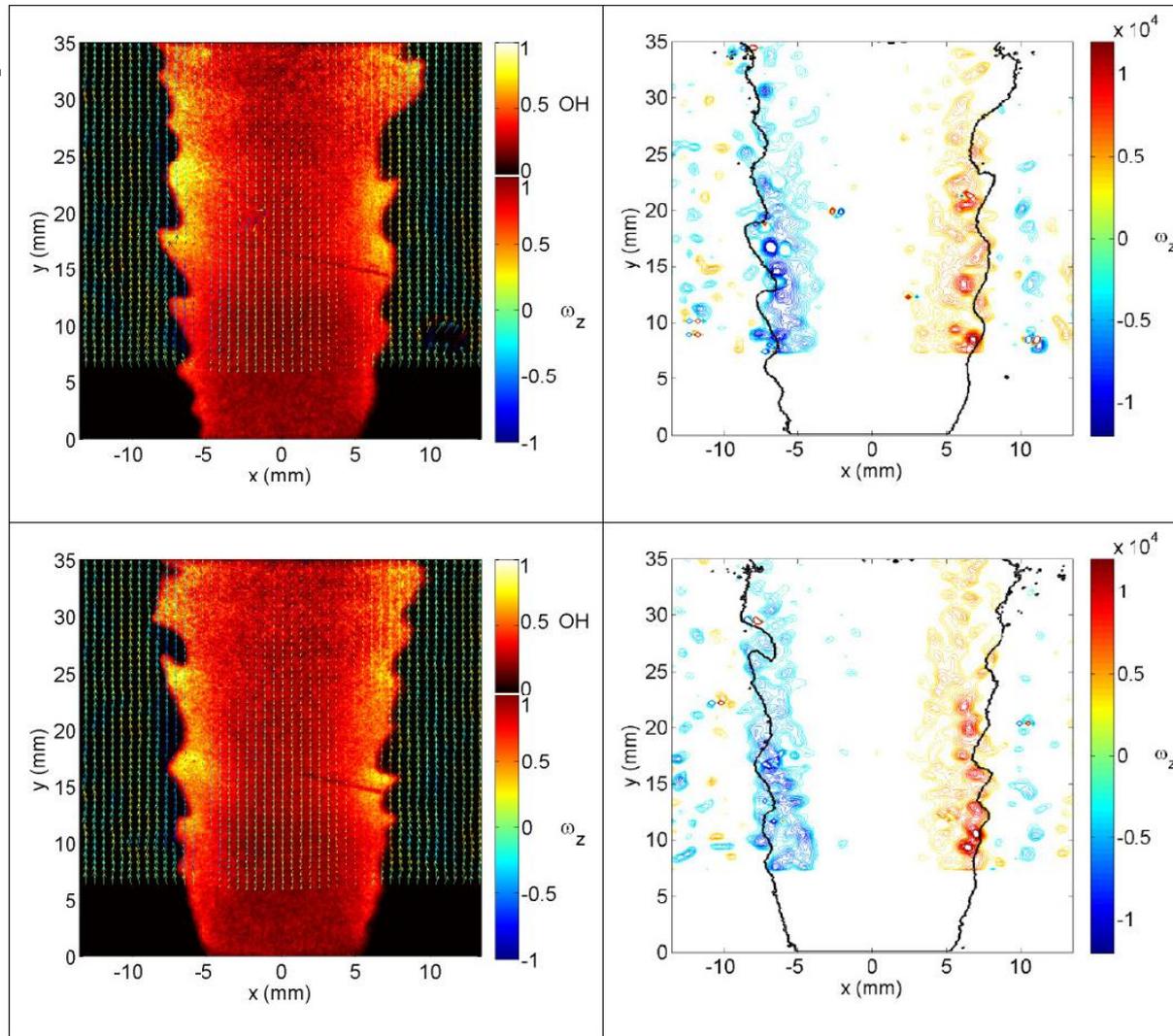
Near blowoff symmetric and asymmetric modes

# Blowoff



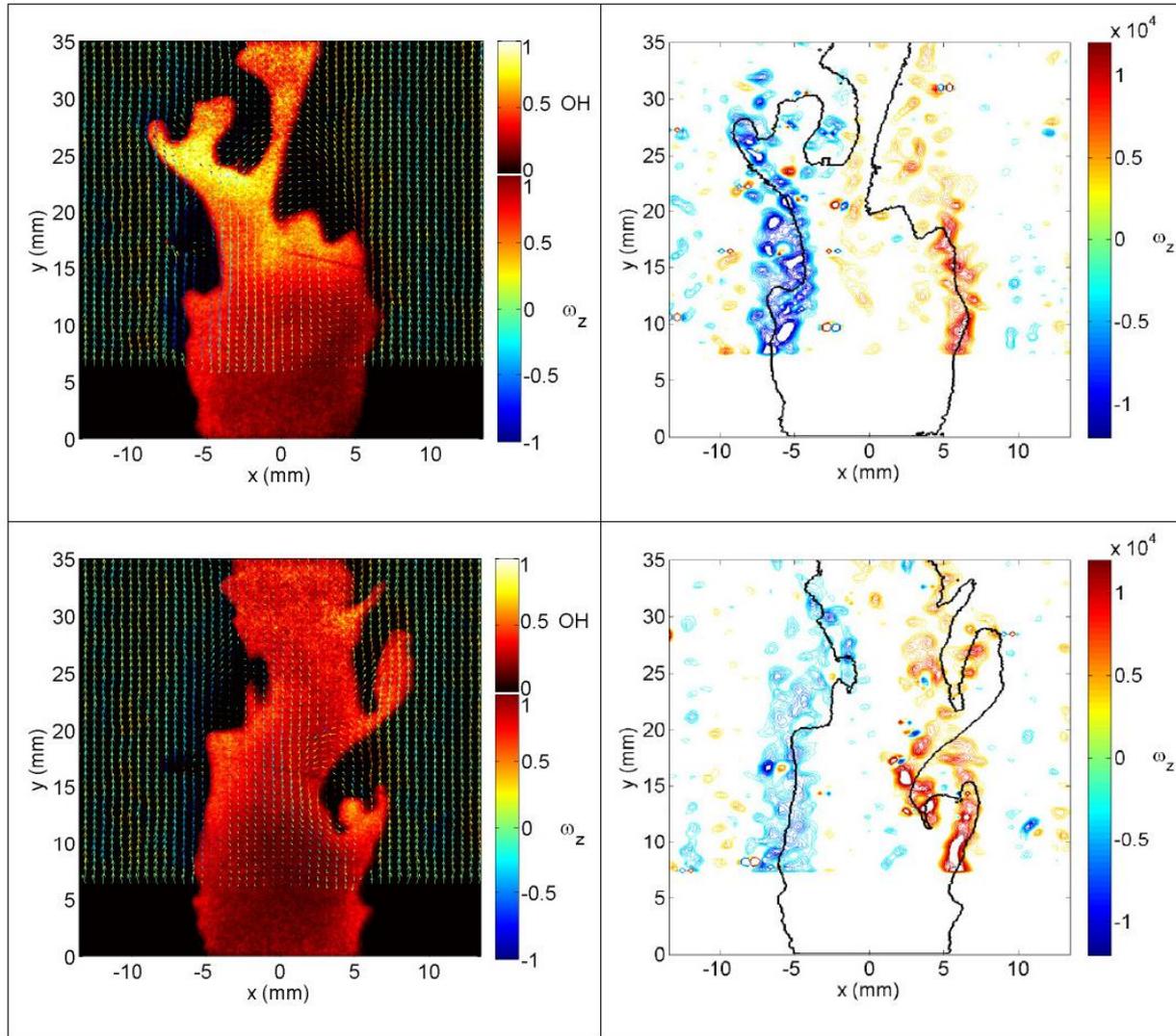
# Simultaneous PIV and OH PLIF

Stable flame at  $\phi = 0.9$



... continued

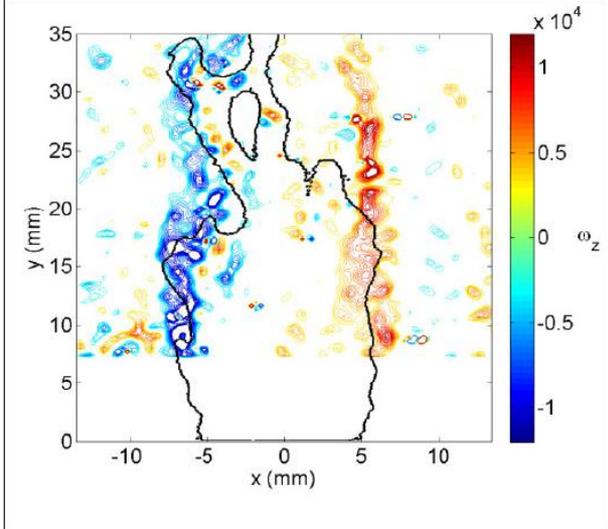
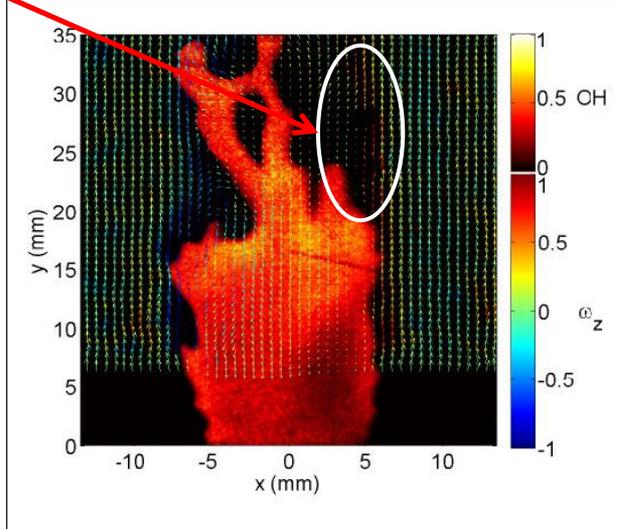
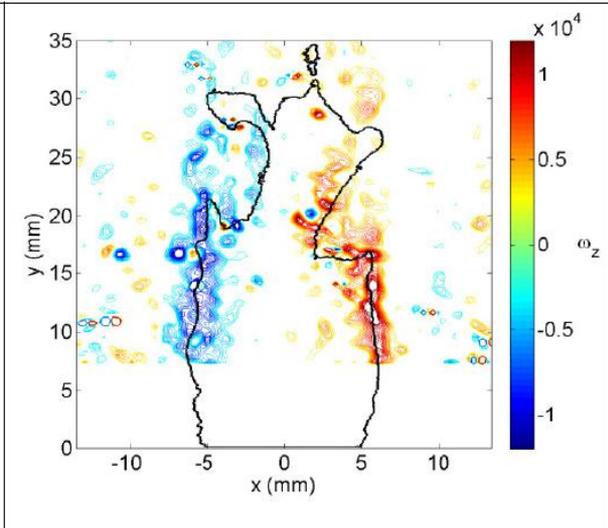
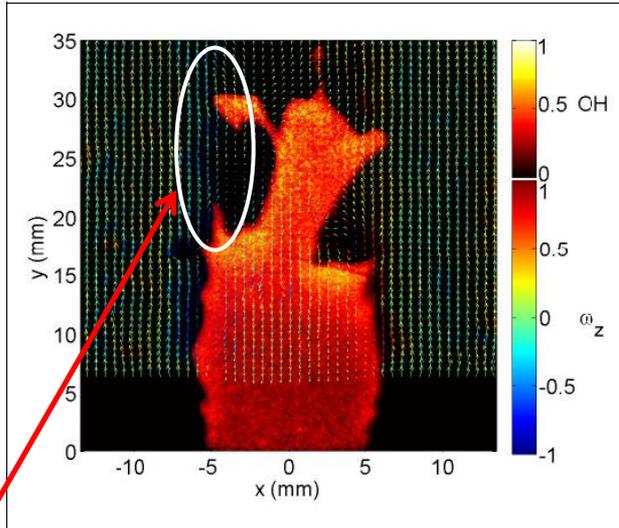
Unstable flame at  $\phi = 0.775$  near blowoff



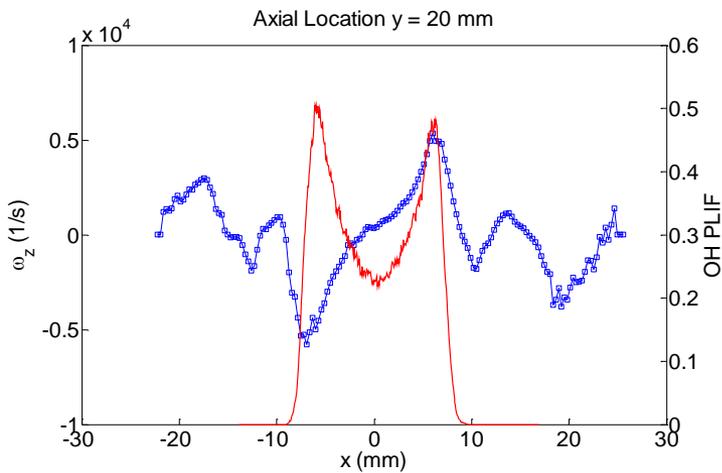
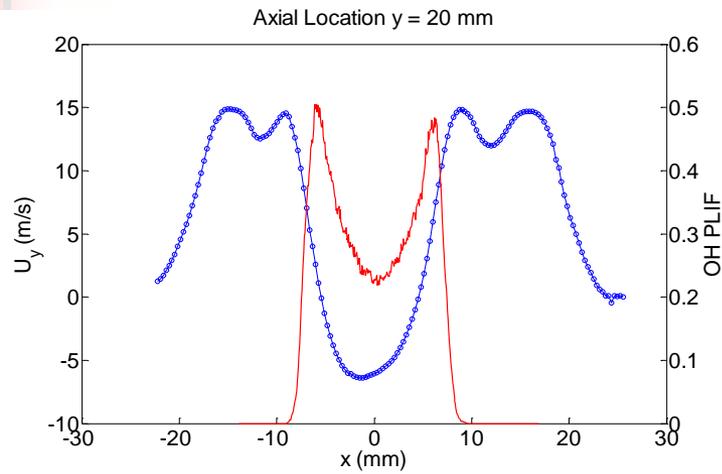


Unstable flame at  $\phi = 0.77$  near blowoff

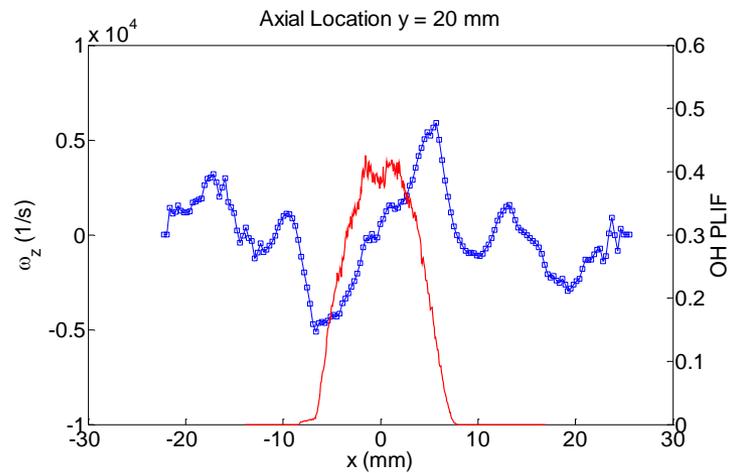
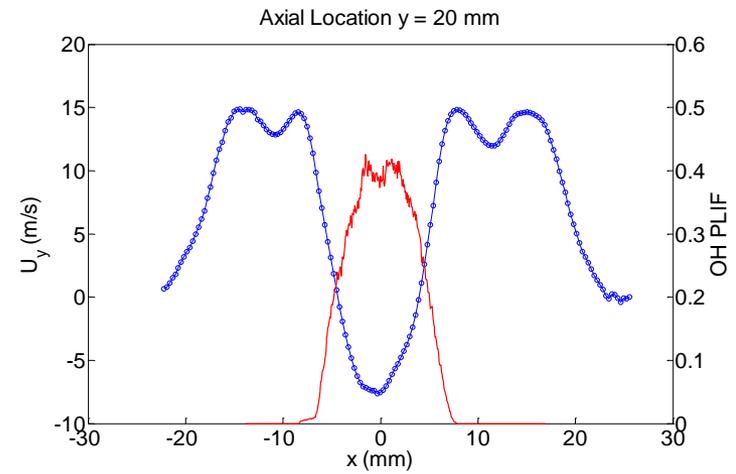
Extinction along shear layers



# Mean $U_y$ and $\omega_z$ superimposed with OH-PLIF

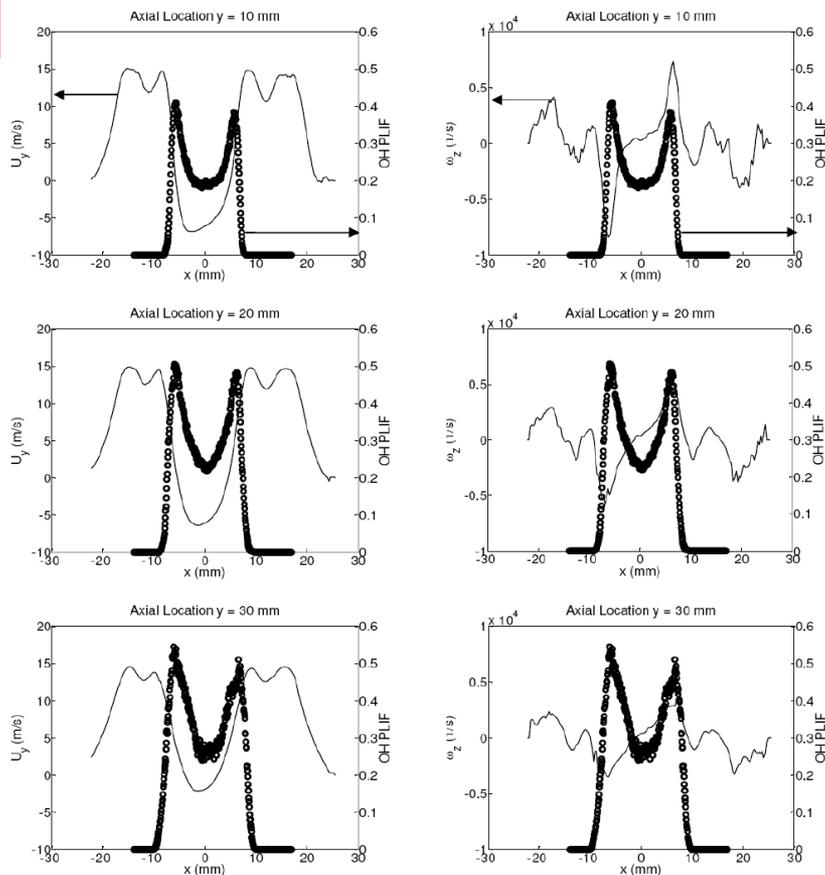


$\phi = 0.90$  : Far from blowoff

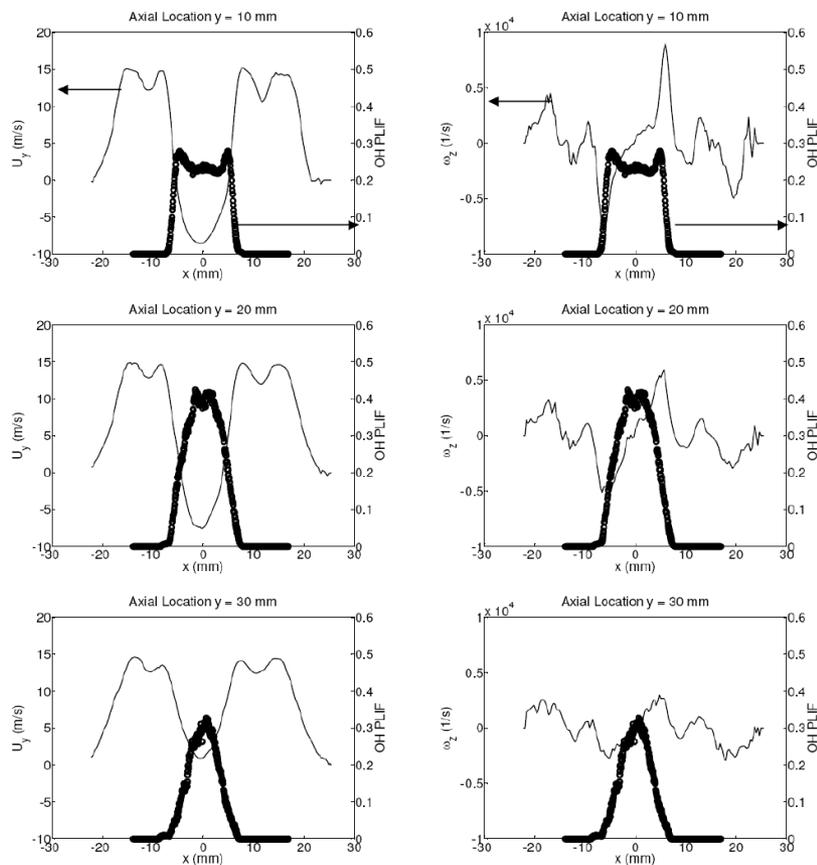


$\phi = 0.77$  : Near blowoff

# Mean $U_y$ and $\omega_z$ superimposed with OH-PLIF



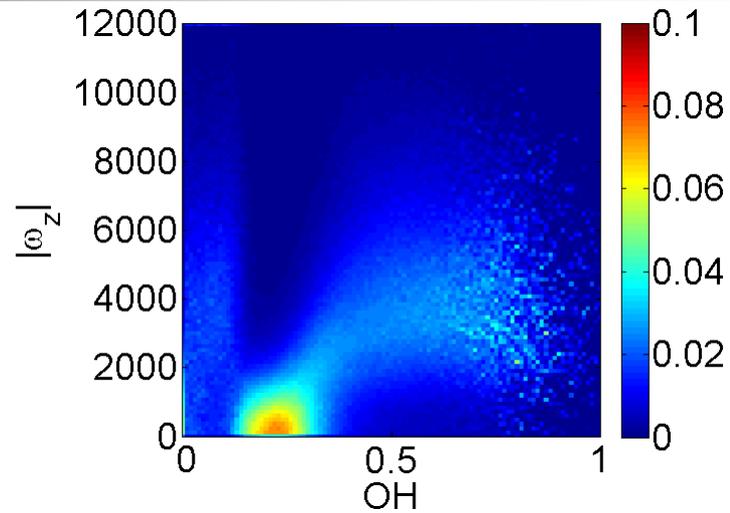
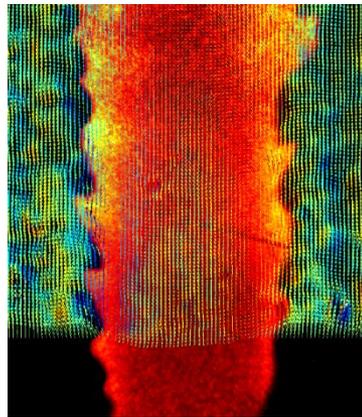
$\phi = 0.90$



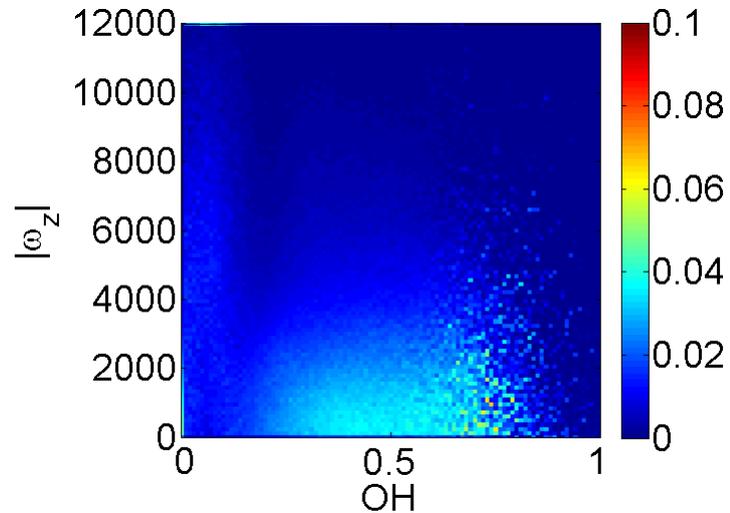
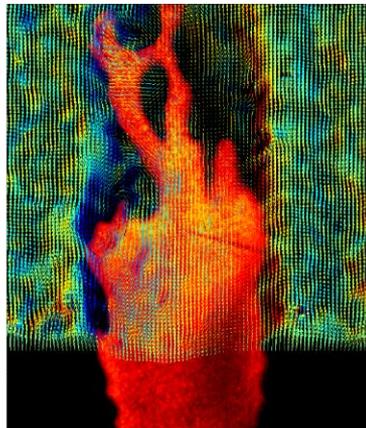
$\phi = 0.77$

# Conditional pdfs : $\text{pdf}(|\omega| | \text{OH})$

$\phi = 0.90$



$\phi = 0.77$



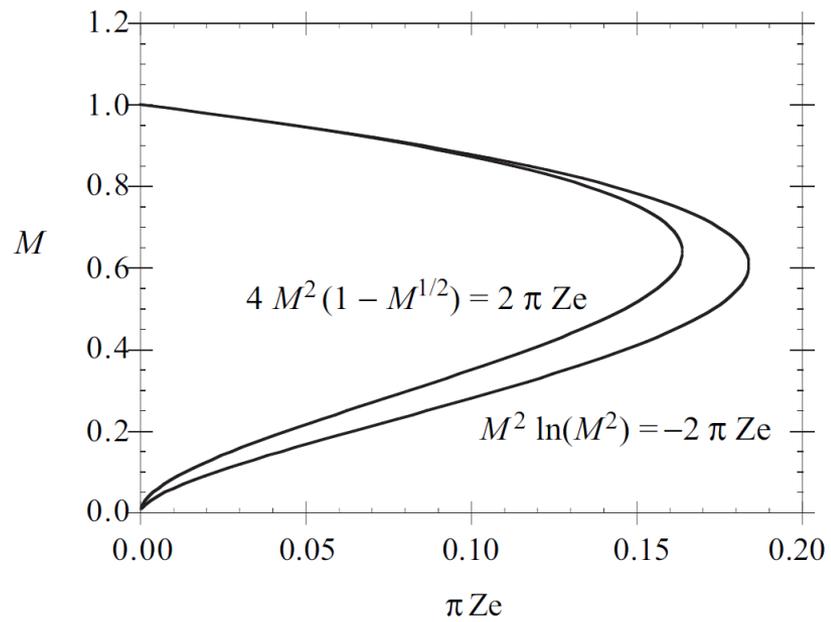
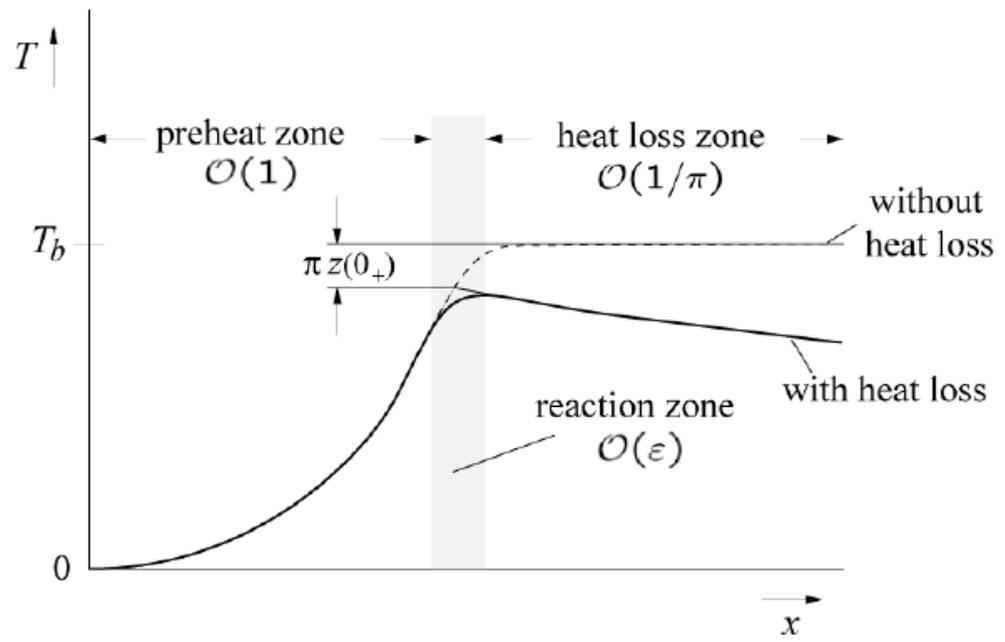


# Basics of Premixed Flame Extinction

1. Extinction by volumetric heat loss
2. Extinction by stretch
  - a.  $Le > 1$
  - b.  $Le < 1$

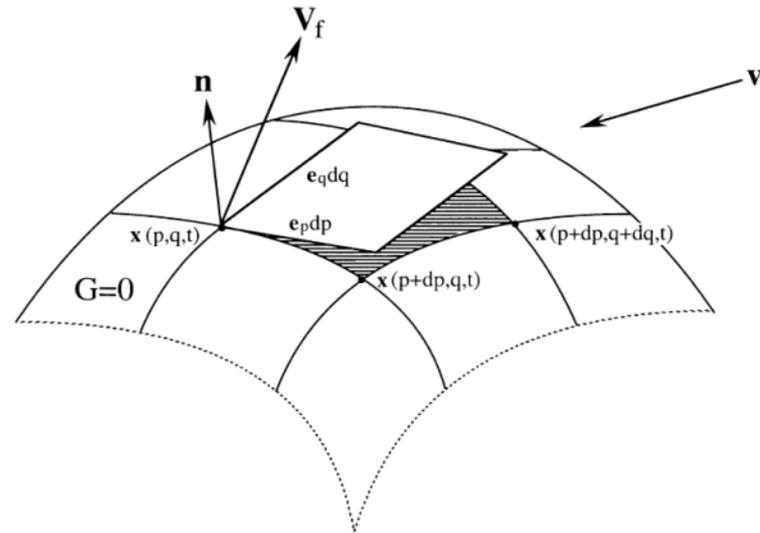
$$\rho_u s_L \frac{dT}{dx} = \frac{d}{dx} \left( \frac{\lambda}{c_p} \frac{dT}{dx} \right) + \frac{Q}{c_p} \omega - \alpha(T - T_u).$$

$$M = \frac{s_L}{s_{L,ref}}$$





# Flame Stretch



generalized form of flame stretch

$$\kappa = \frac{1}{A} \frac{dA}{dt} = \underbrace{\underbrace{S_L C}_{\text{stretch rate by pure curvature}} - \underbrace{(\mathbf{v} \cdot \mathbf{n})c}_{\text{normal strain } \kappa_n}}_{\text{stretch rate by curvature}} + \underbrace{\nabla_t \cdot \mathbf{v}_t}_{\text{tangential strain } \kappa_s}$$

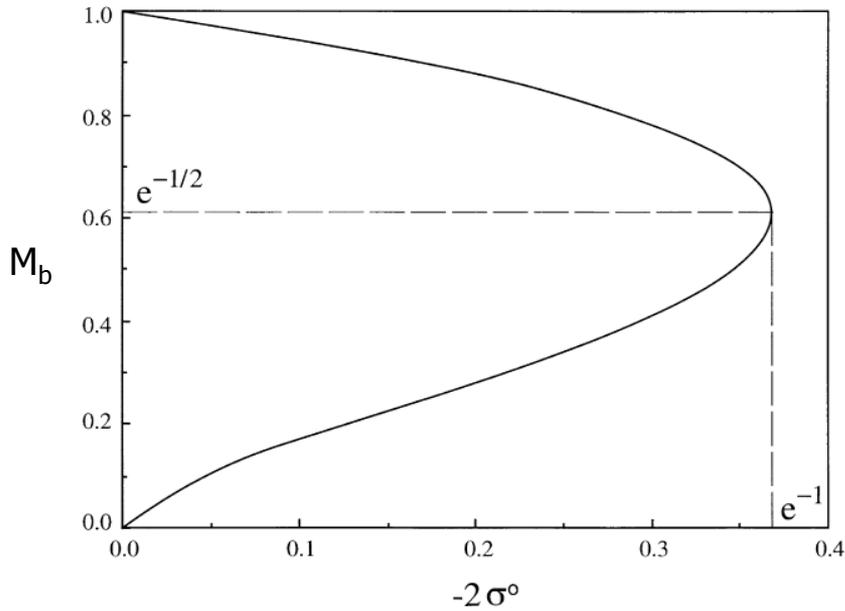
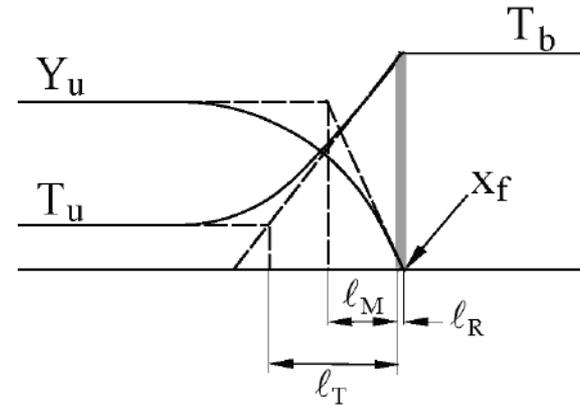
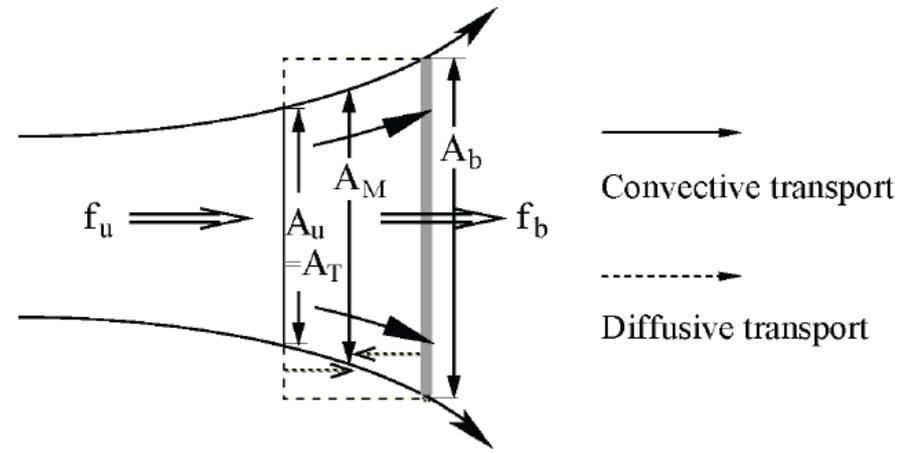
Tangential straining part of flame:

$$\kappa_s = (\delta_{ij} - n_i n_j) S_{ij}$$

$$\kappa_{s,2D} = -n_x \times n_y \times \left( \frac{\partial u}{\partial y} + \frac{\partial v}{\partial x} \right) + (1 - n_x^2) \times \frac{\partial u}{\partial x} + (1 - n_y^2) \times \frac{\partial v}{\partial y}$$



# Stretch Effects



$$M_b^2 \ln M_b^2 = 2\sigma^0$$

$$\text{where } \sigma^0 = \frac{Ze^0}{2} \left( \frac{1}{Le} - 1 \right) Ka^0$$

All HC flames except methane are  $Le > 1$

$$Ze = \frac{E_a}{R^0 T_{\max}^2}$$

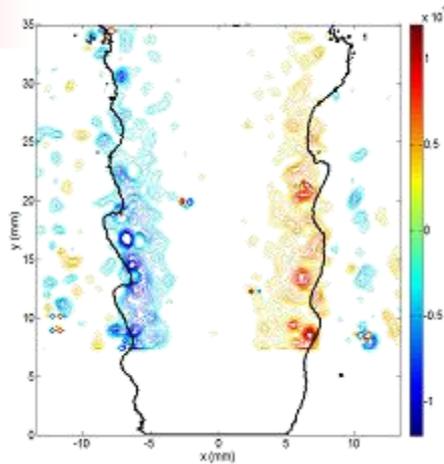
$$Le = \frac{\alpha}{D}$$

$$Ka = \frac{l_T}{S_u} \kappa$$

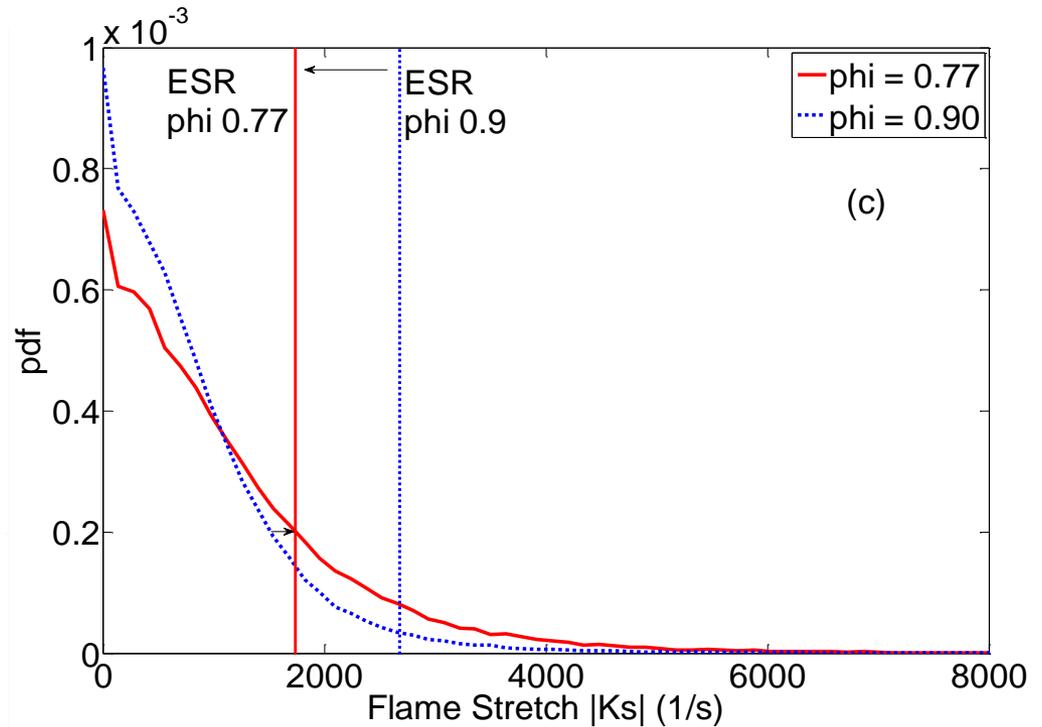
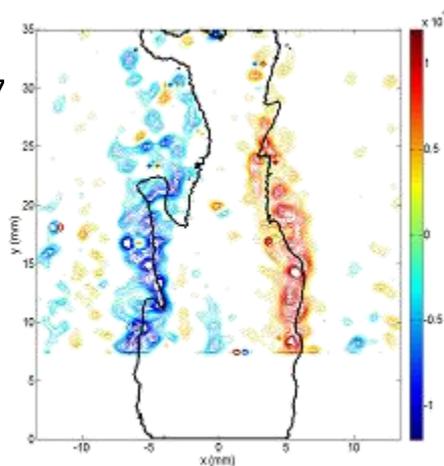
# Mean pdfs of strain rate along OH PLIF edge



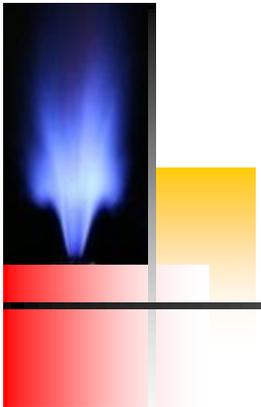
$\phi = 0.90$



$\phi = 0.77$

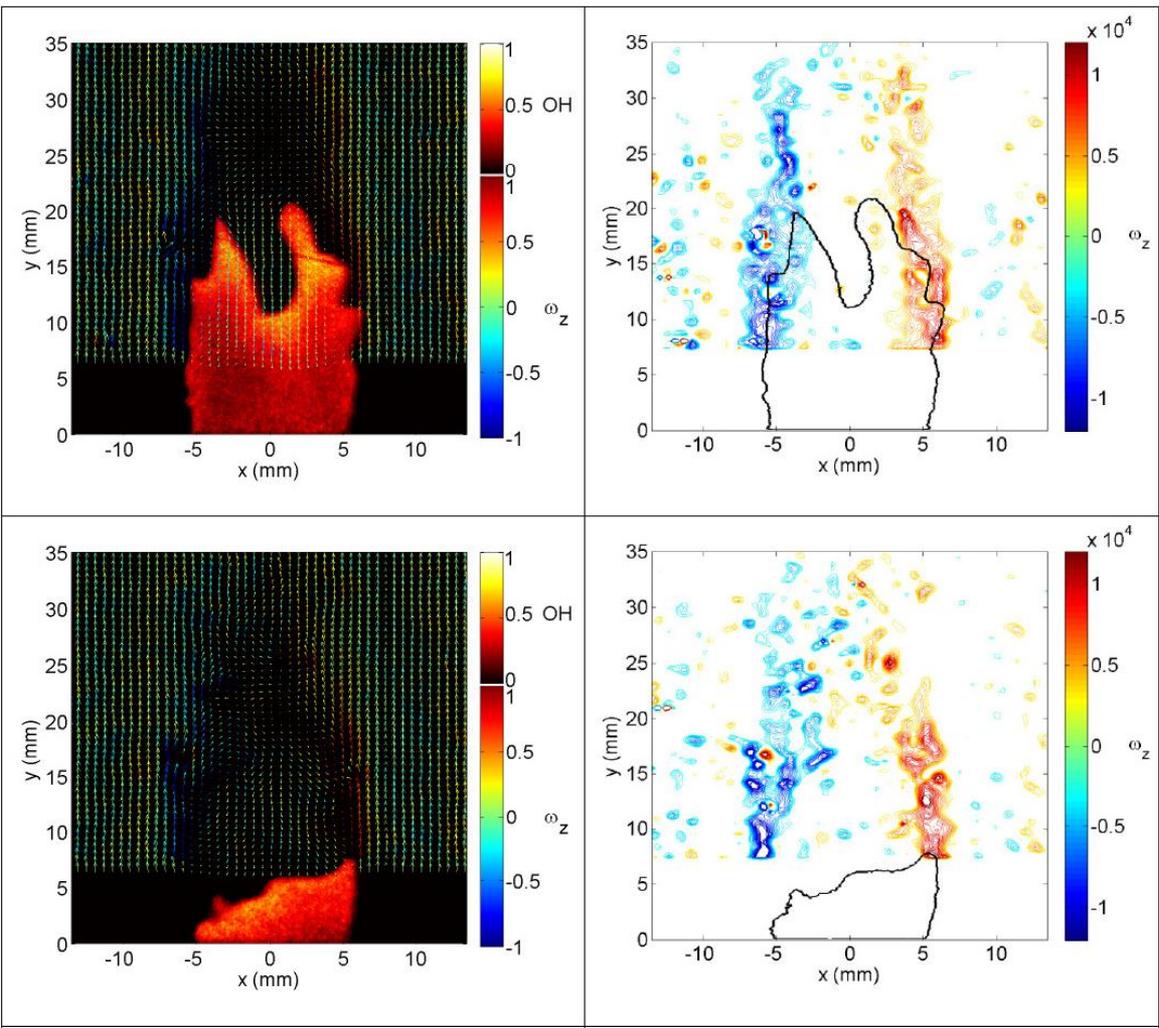


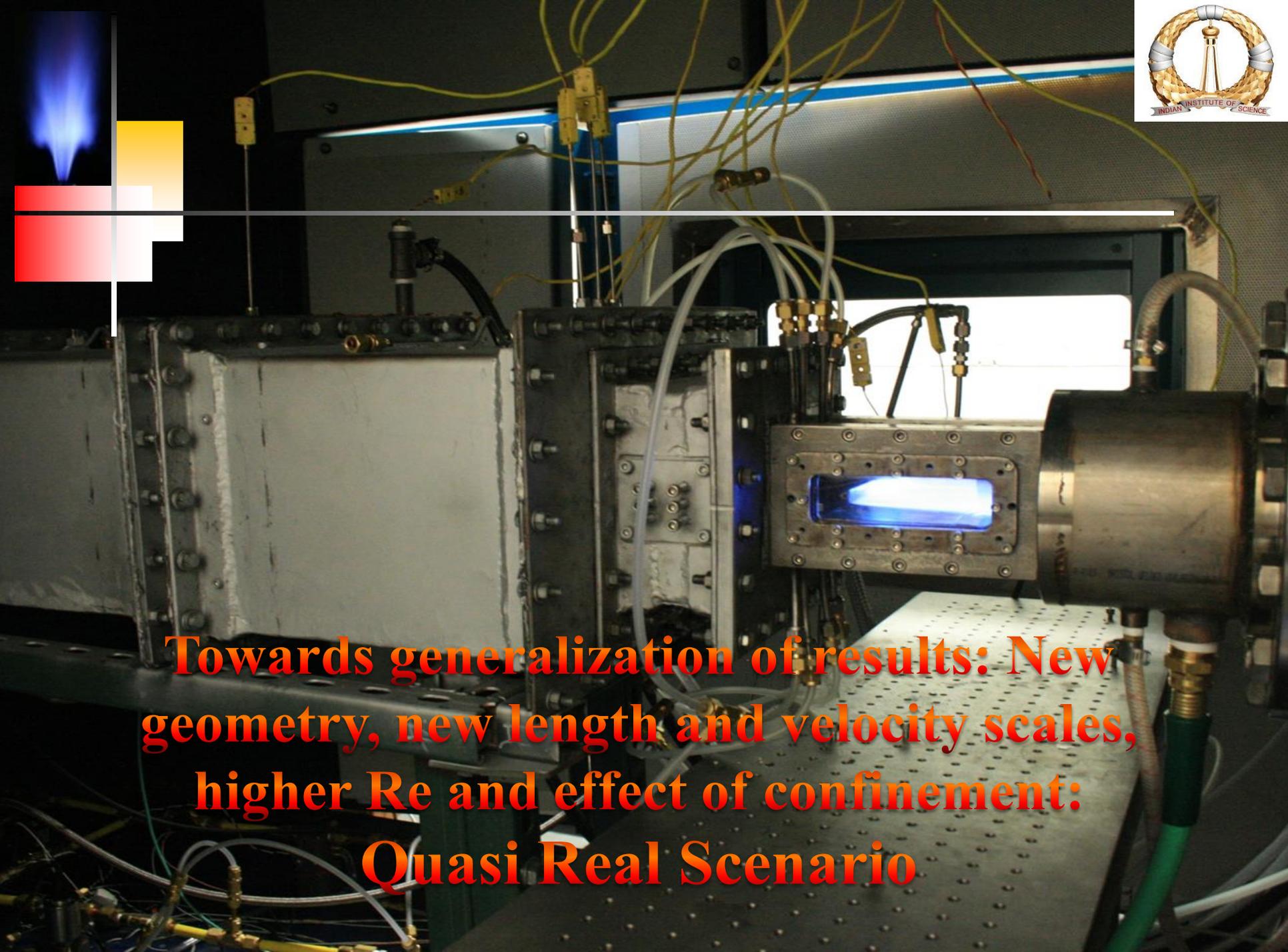
Limiting condition created by  $\kappa_{\text{flame}}$  and  $\kappa_{\text{esr}}$  shifting in opposite directions with reducing  $\phi$ .



### Stage 3 in blowoff dynamics

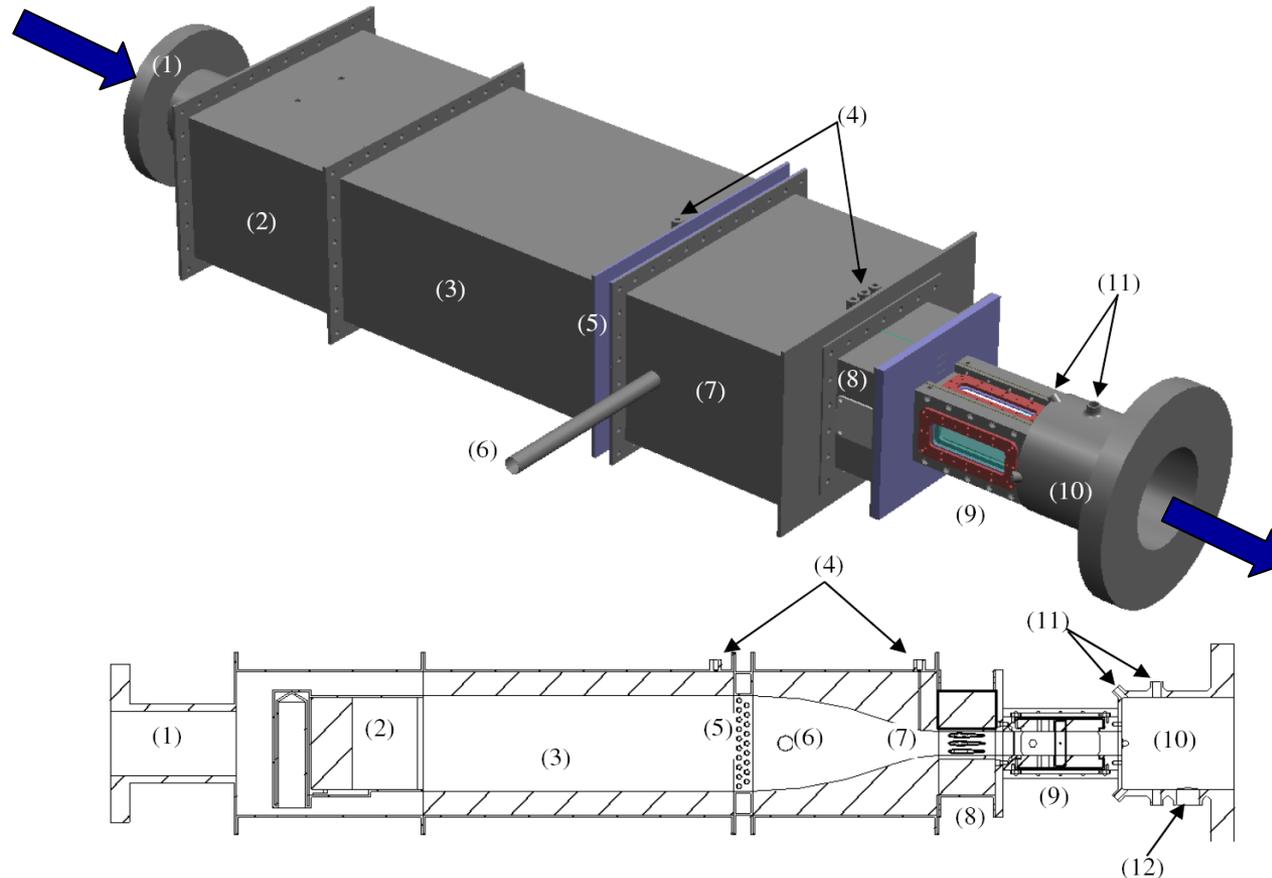
Recirculation zone burn





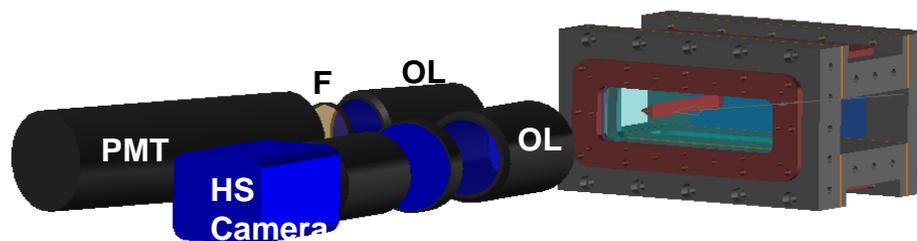
**Towards generalization of results: New geometry, new length and velocity scales, higher  $Re$  and effect of confinement: Quasi Real Scenario**

# The UConn Rig

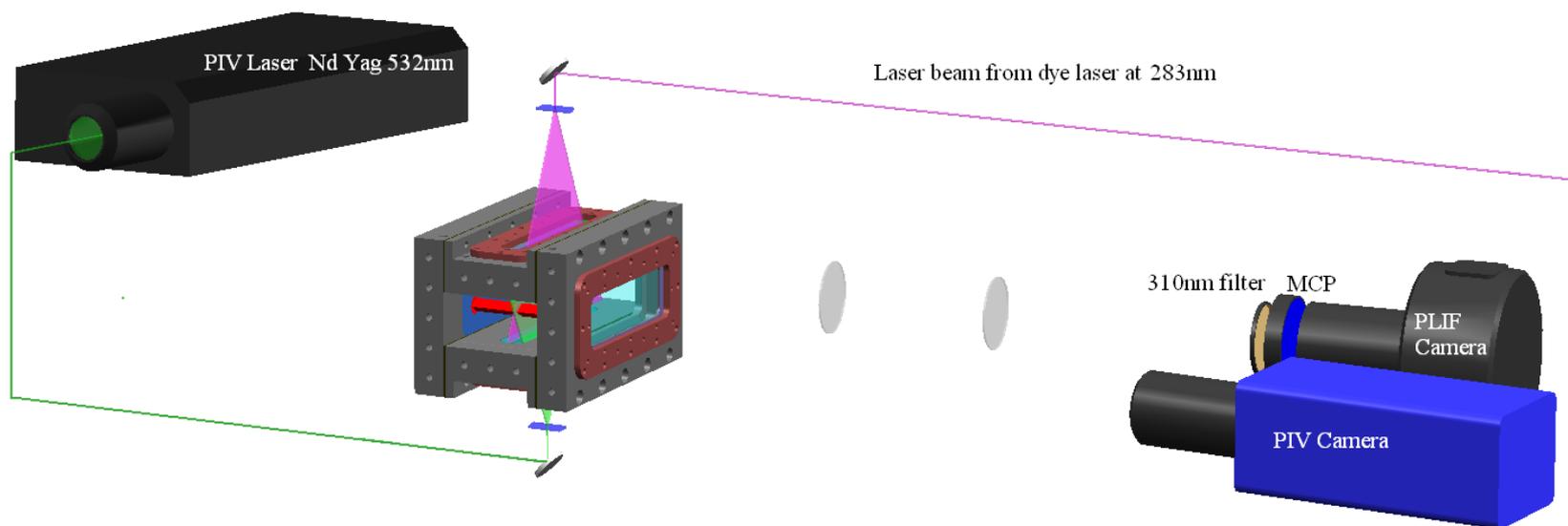


Layout of experimental rig. (1): Air inlet, (2): Maxon NP-LE burner, (3): Settling Duct, (4): Thermocouple Ports, (5): Heat exchanger, (6): PIV-Seeded air inlet, (7): Convergent nozzle, (8): Fuel injectors, (9): Optically accessible test burner, (10): Dump duct, (11): Water nozzle ports, (12): Water drain. (image courtesy: Steven Tuttle)

# Experimental Setup

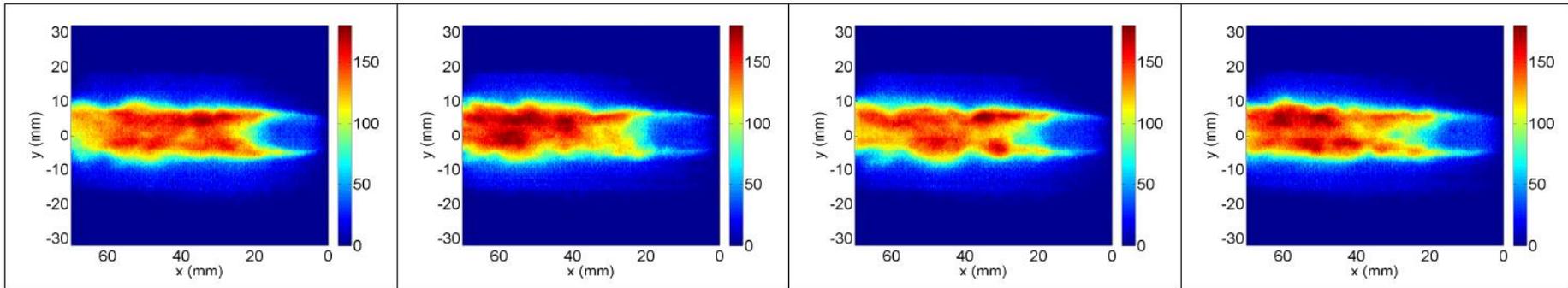


Imaging setup



Simultaneous PIV PLIF setup

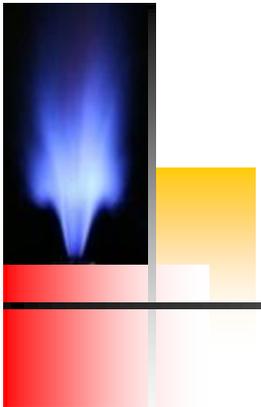
# Stable Flame at $\phi = 0.85$



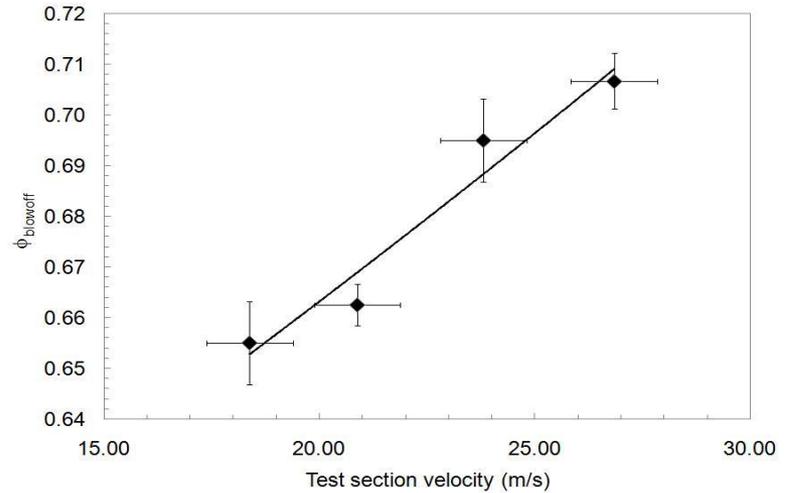
High speed chemiluminescence emission images for a stable flame very far from blowoff for  $U_m = 18.3$  m/s at  $\phi = 0.85$  at 500 frames per second and  $100 \mu\text{s}$  exposure.



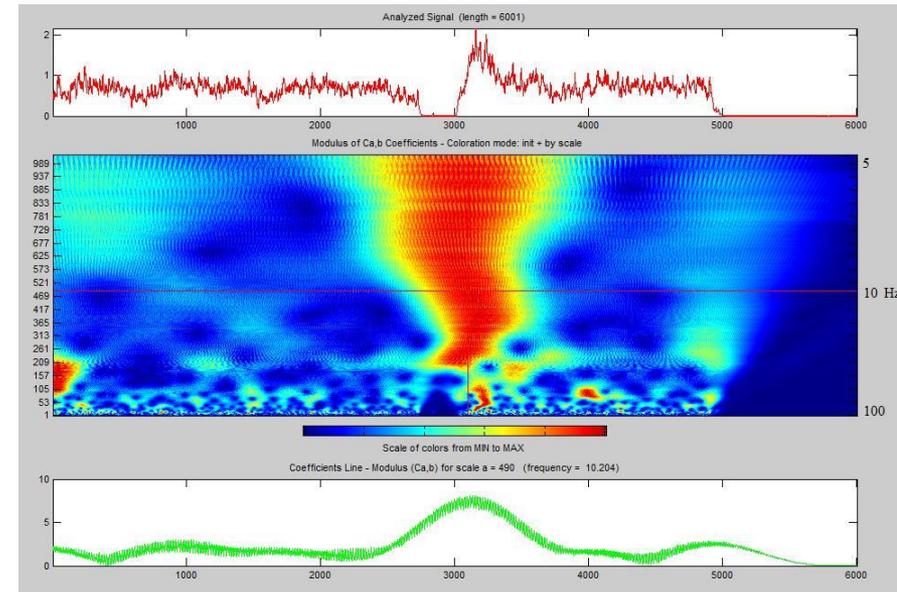
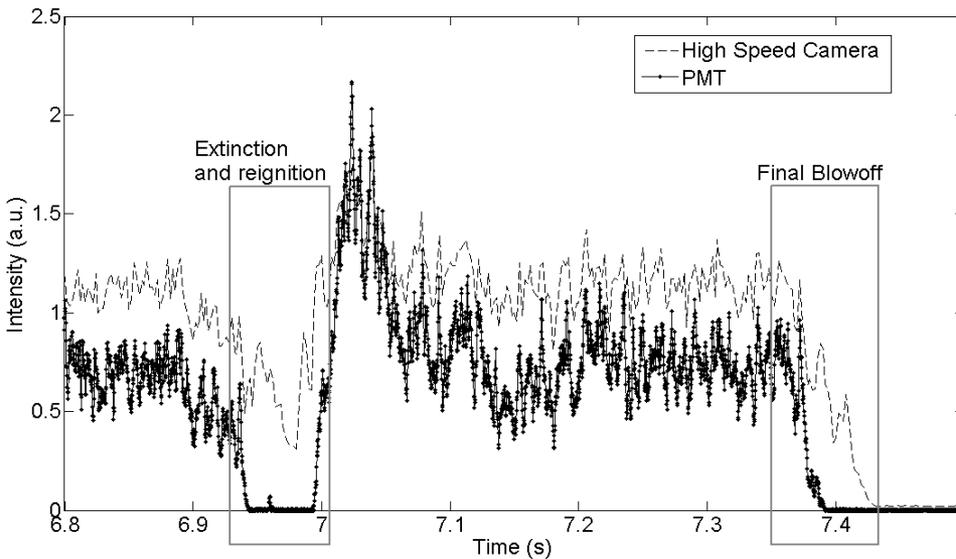
# Blowoff and near blowoff dynamics



Blowoff curve



Time history of chemiluminescence near blowoff



Wavelet Analysis can be a powerful predictive tool for developing an in situ sensor



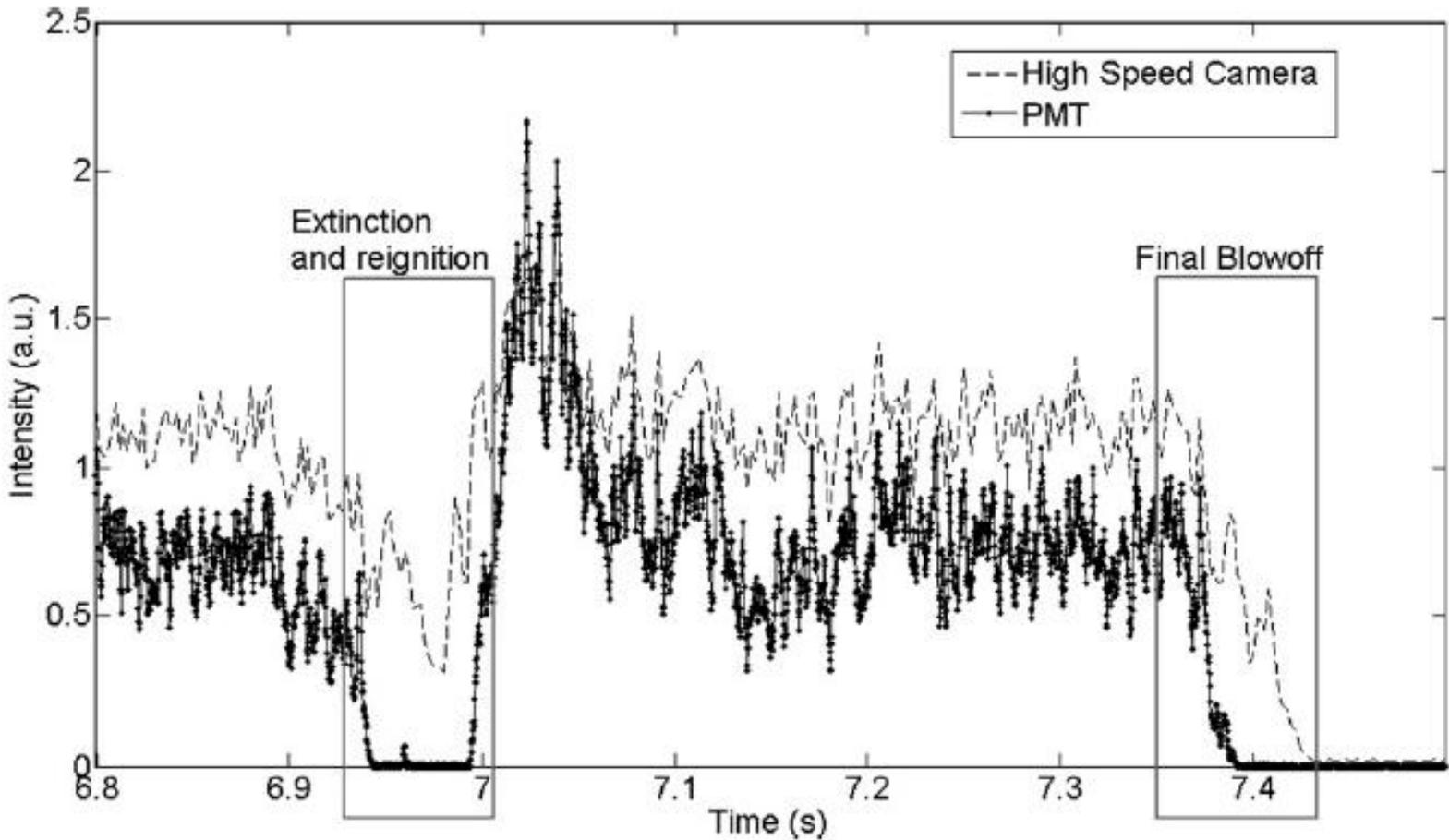
# Extinction reignition and blowoff : movie



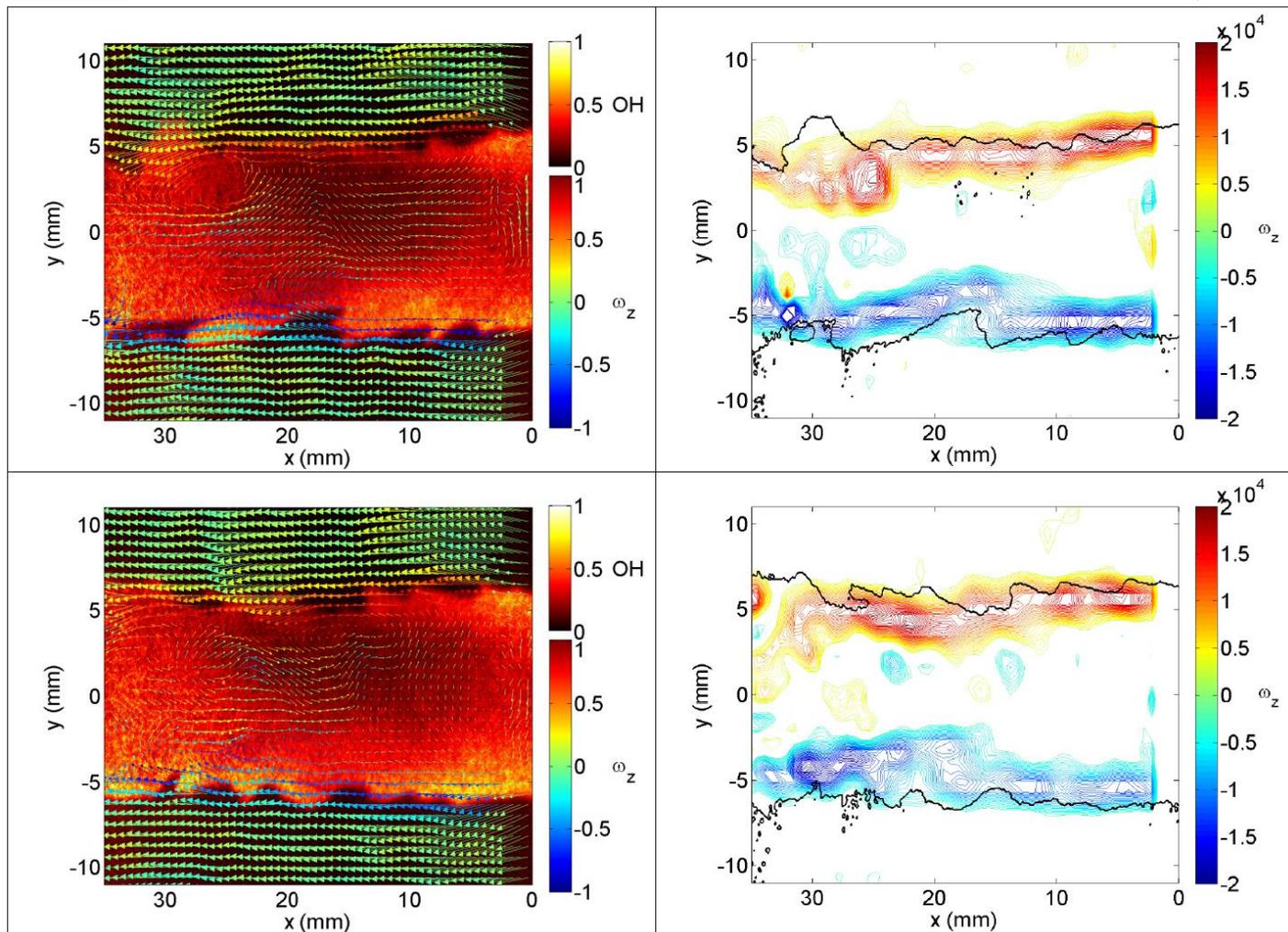
Extinction and Reignition



# Camera (whole); PMT (wake)

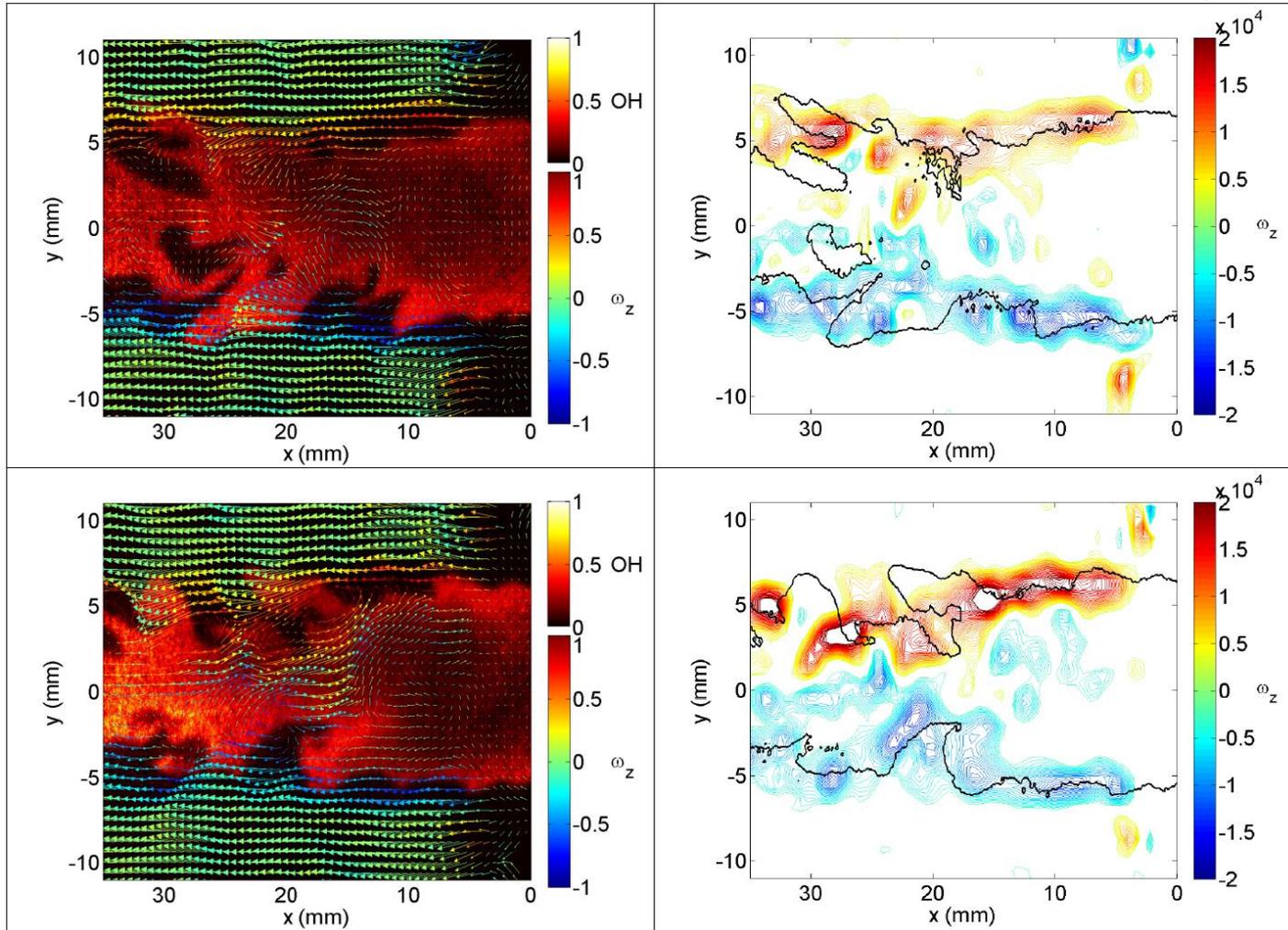


# Simultaneous PIV and OH PLIF



Stable flame  
 $\phi = 0.85$

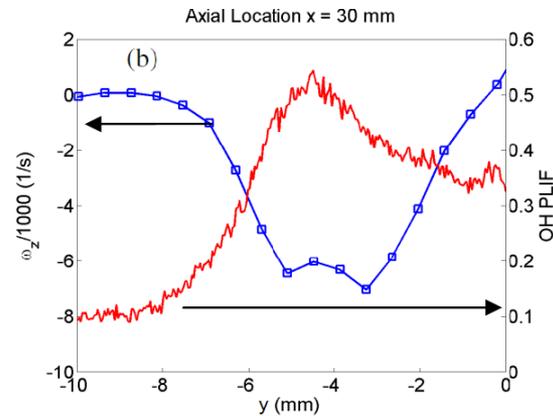
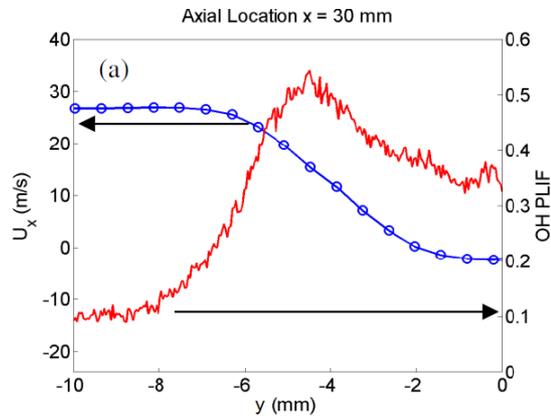
# Extinction along shear layers



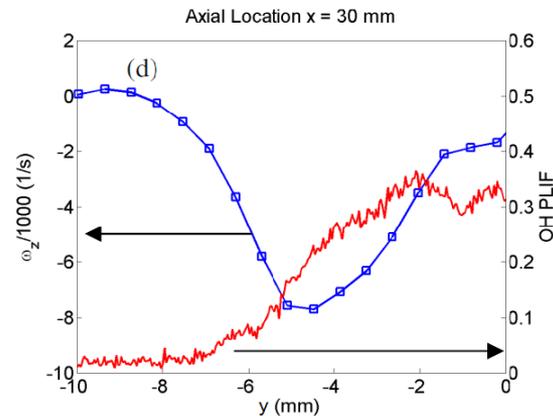
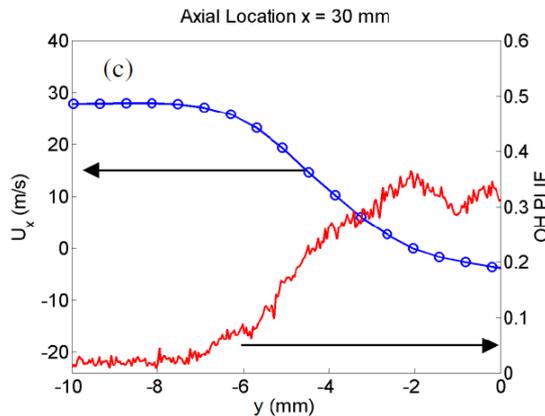
Near blowoff  
flame  
 $\phi = 0.65$

# Mean profiles of $U_x$ , $\omega_z$ and OH

$\phi = 0.85$

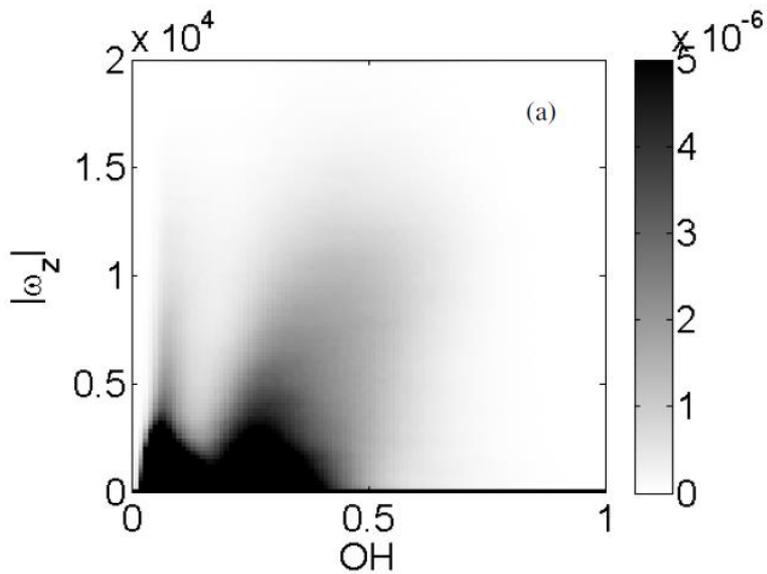


$\phi = 0.65$

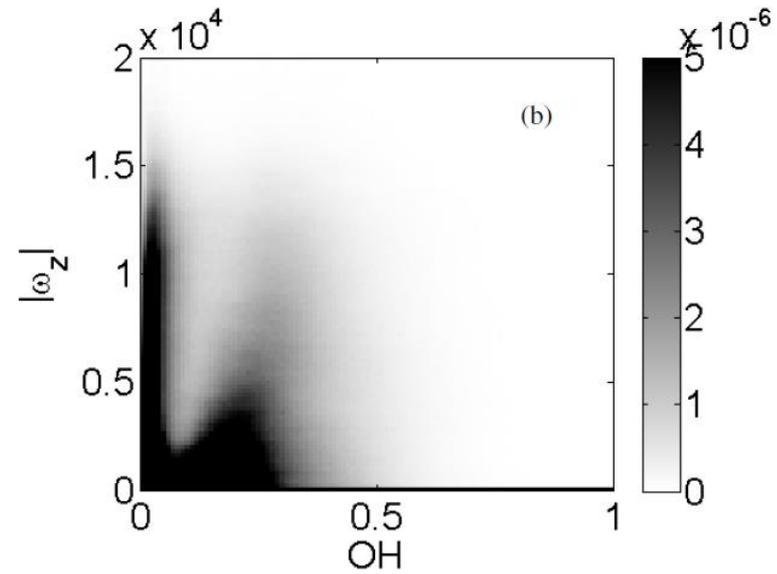


Left panels: Mean axial velocity from PIV superimposed with OH fluorescence signal from PLIF.  
 Right panels: Mean out of plane vorticity superimposed with OH fluorescence, both at axial locations of 30 mm for  $\phi = 0.85$  (a,b) and for  $\phi = 0.65$  (c,d).

# Joint probability density functions

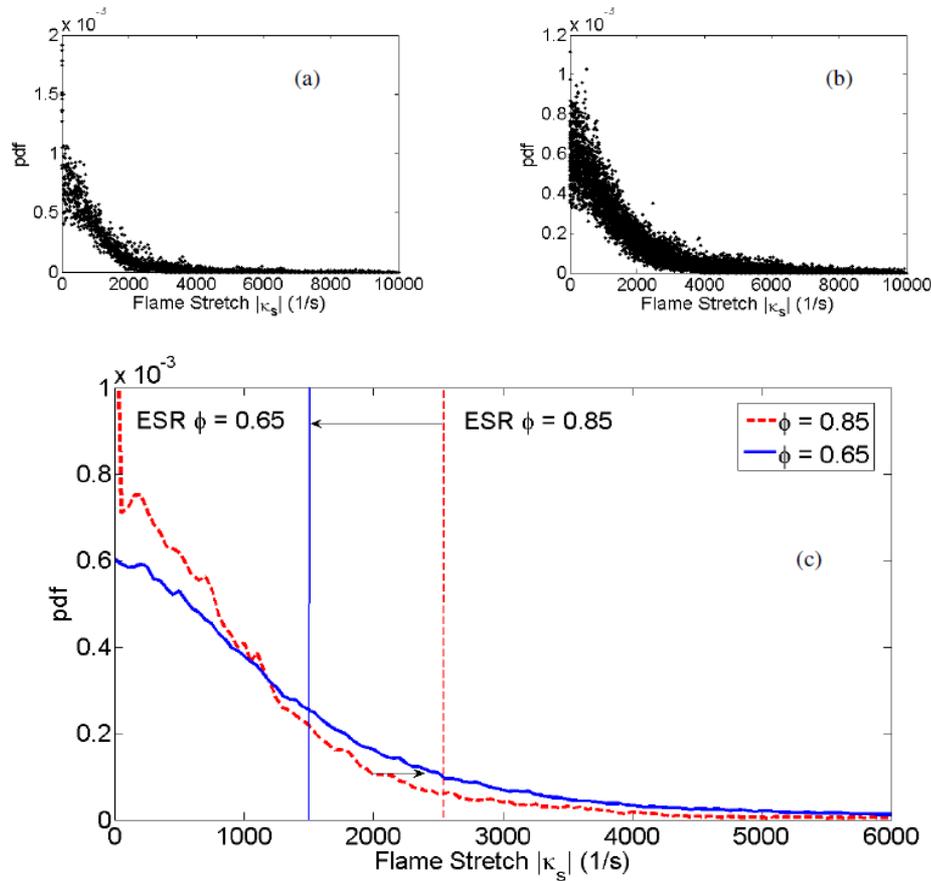


(a)  $\phi = 0.85$  (far from blowoff)



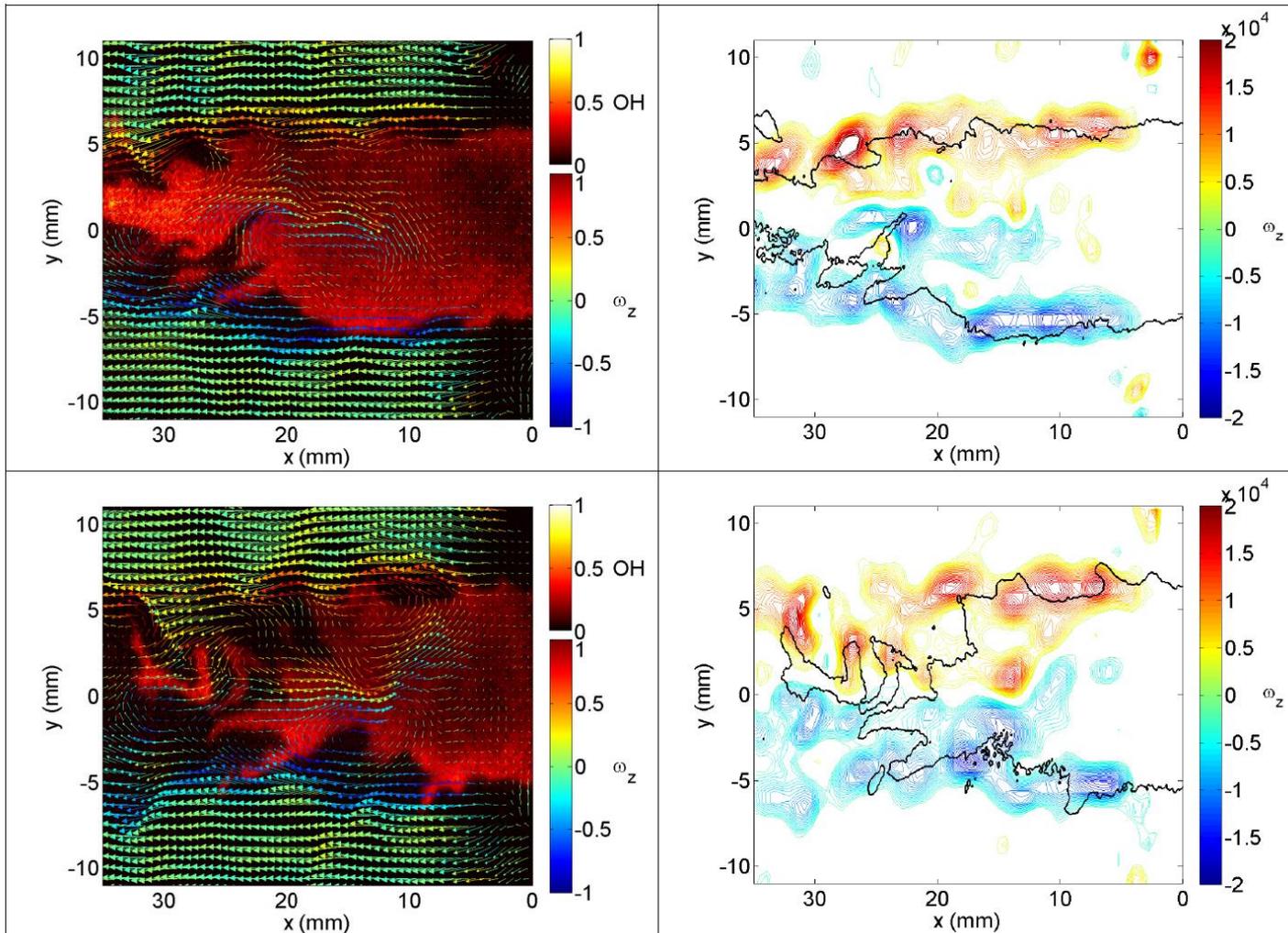
(b)  $\phi = 0.65$  (near blowoff)

# Stretch Rate Pdf



Probability density function of  $|K_s|$  at (a)  $\phi = 0.85$  (b)  $\phi = 0.65$  and (c) Mean pdfs of  $|K_s|$  at  $\phi = 0.85$  and  $\phi = 0.65$ .

# Extinction along shear layers and recirculation zone burn



Near blowoff  
flame  
 $\phi = 0.60$

# Proposed blowoff mechanism

Towards blowoff  $\phi \downarrow$  and hence  $S_L \downarrow$ , so flame shifts from outside towards the shear layer vortices. Partial flame extinction along shear layers due to  $\kappa_{\text{flame}} > \kappa_{\text{extinction}}$  by convecting vortices.

Non reacting unburnt mixture entrains into RZ and due to favorable flow time scales reacts within RZ. Hence OH and chemiluminescence

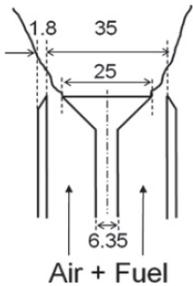
Reacting RZ reignites the shear layers to cause reignition

Reacting RZ fails to reignite the shear layers

More parts of the shear layers become “cold” Absolute instability : Asymmetric mode steps in to cause greater perturbations

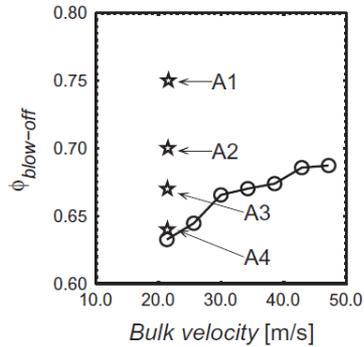
Blowoff

# Works at Cambridge: lean CH<sub>4</sub>-air flames

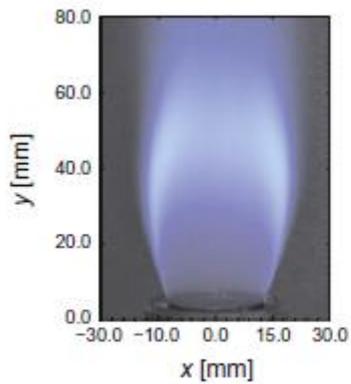
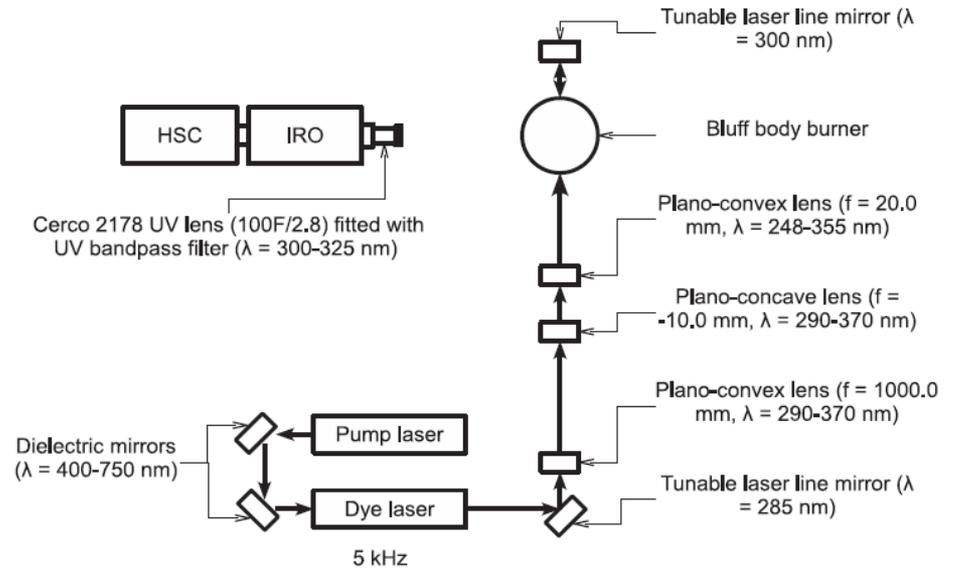


Air + Fuel

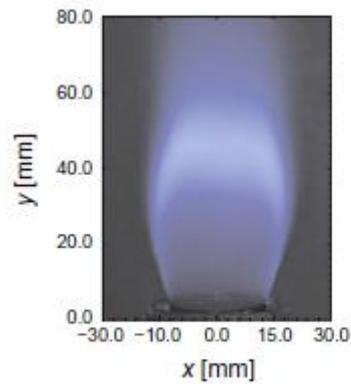
(a)



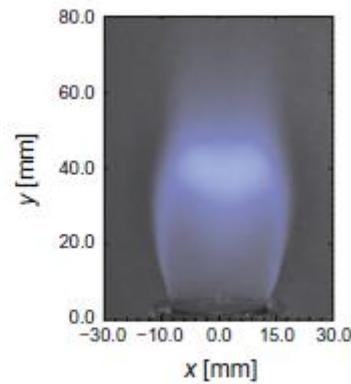
(b)



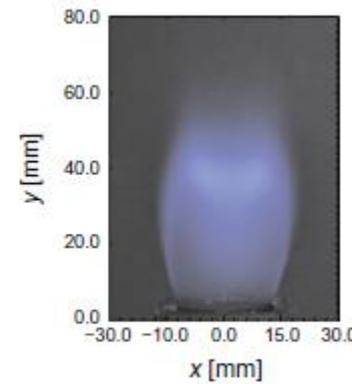
(a) A1



(b) A2

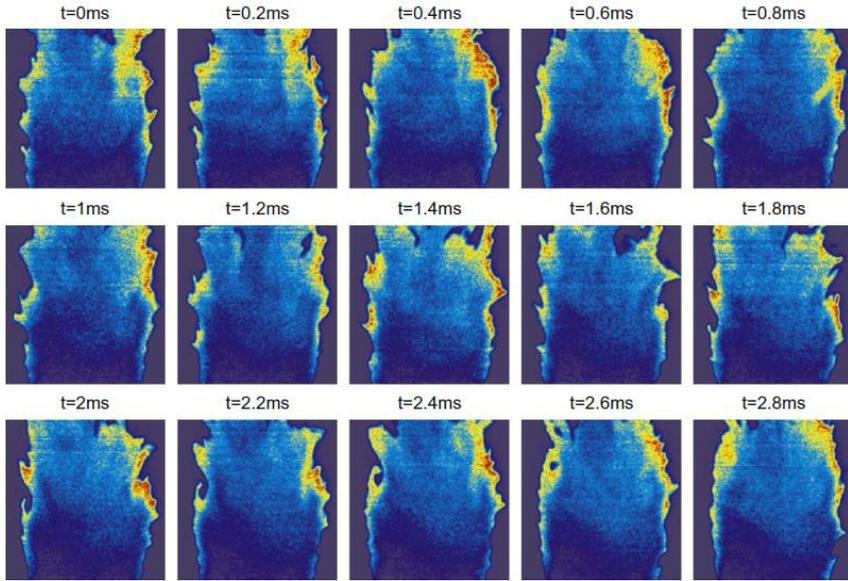


(c) A3



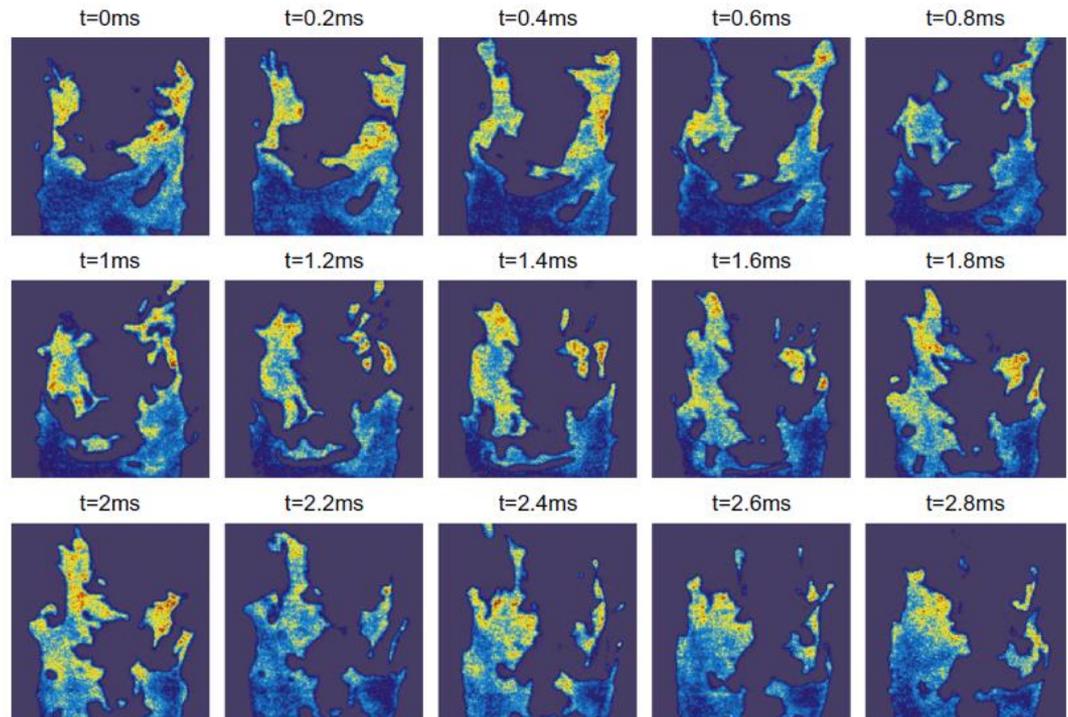
(d) A4

# OH PLIF



(a)

Far from blowoff



Near blowoff

(b)

# Blowoff in Vitiated Flows

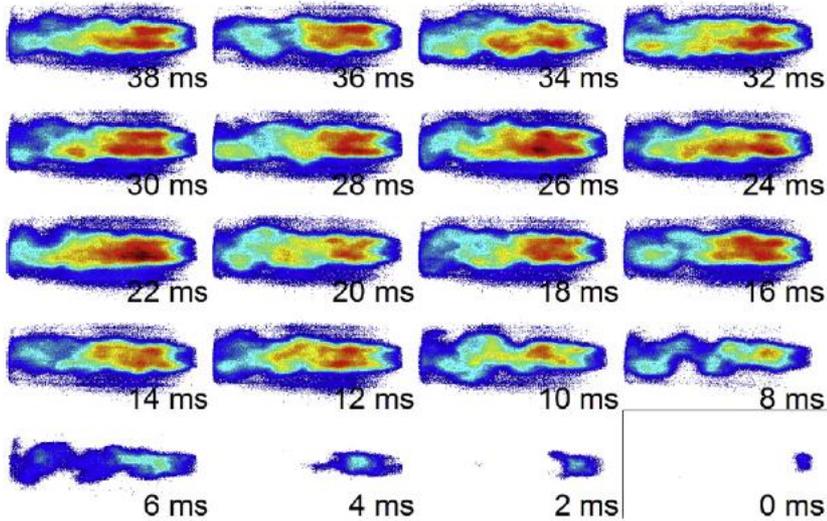


Fig. 9. High-speed chemiluminescence images of a blowoff event at  $\phi_T = 0.51$ ,  $\phi_P = 0.15$ , and 59 m/s, gathered at 500 frame/s.

Vitiated

Unvitiated

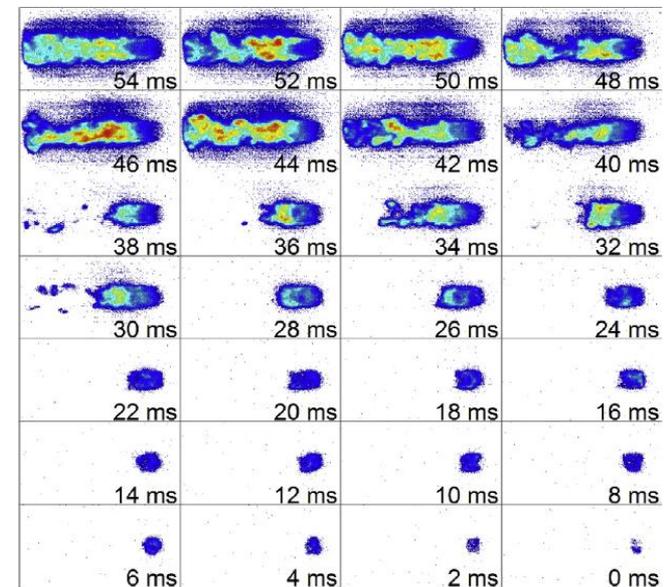
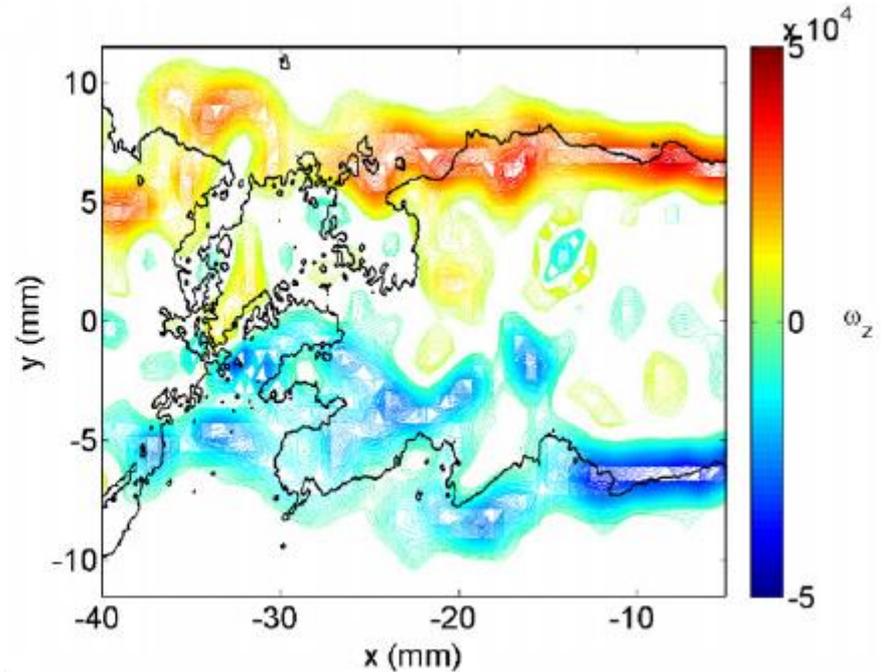
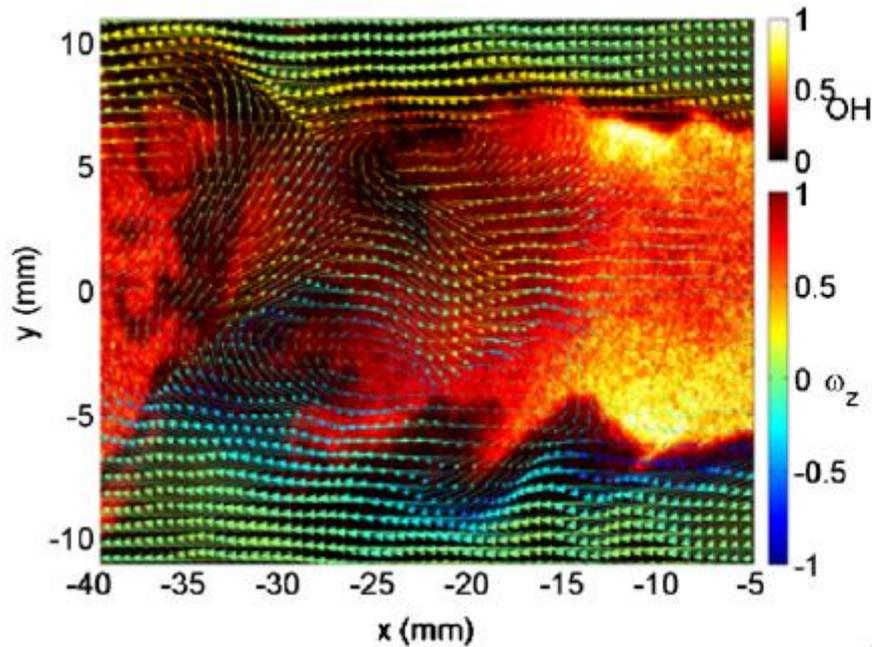


Fig. 10. High-speed chemiluminescence images of a blowoff event at  $\phi = 0.65$ ,  $\phi_P = 0.00$ , and 18.5 m/s, gathered at 500 frames/s.

# PIV-PLIF of near blowoff vitiated flames



Significant difference between vitiated and unvitiated blowoff

# Forced blowoff mechanism

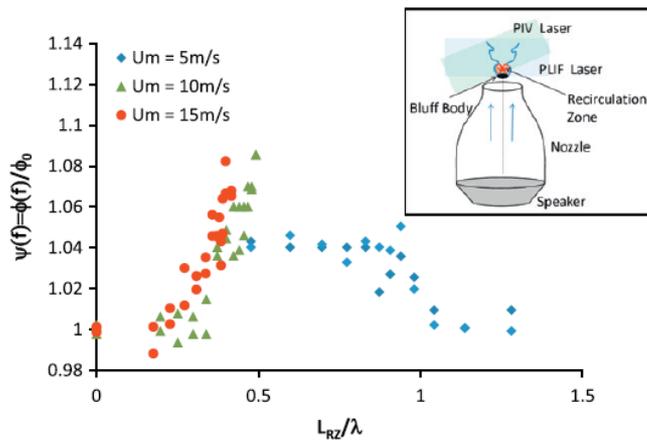
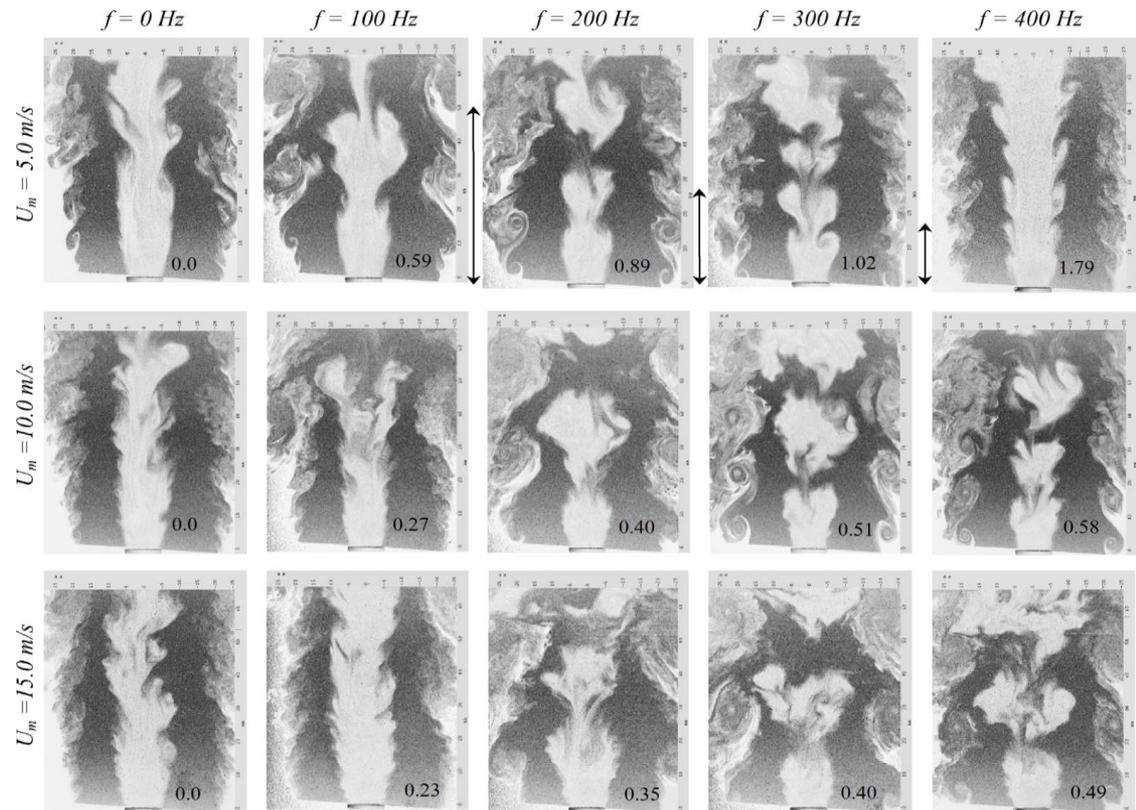
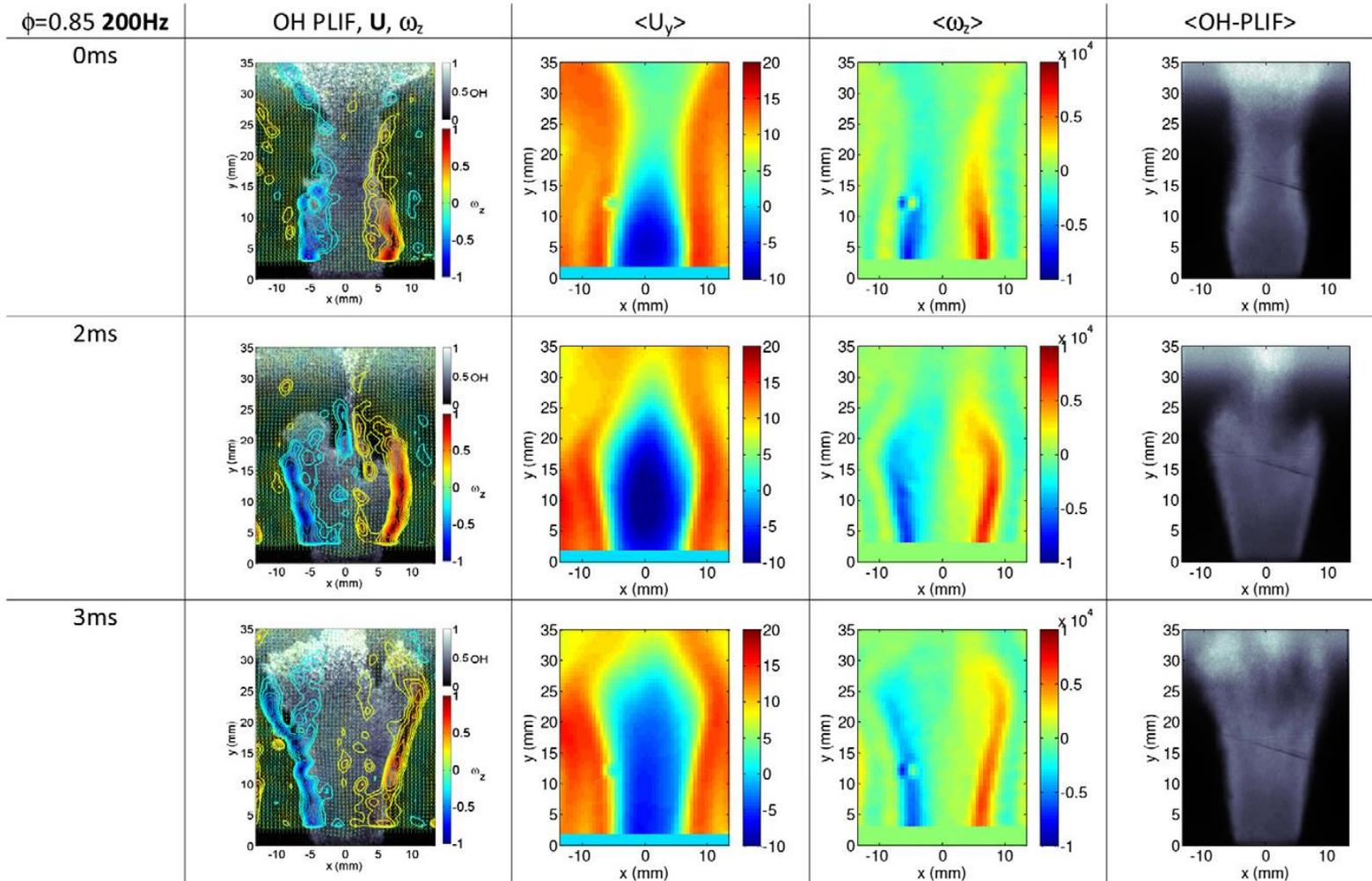


Fig. 1. Ratio of blowoff equivalence ratio at a particular frequency of perturbation with blowoff equivalence ratio at no perturbation as a function of the ratio of  $L_{RZ}/\lambda$  for  $U_m = 5, 10$  and  $15$  m/s. A schematic of the burner is shown in the inset.



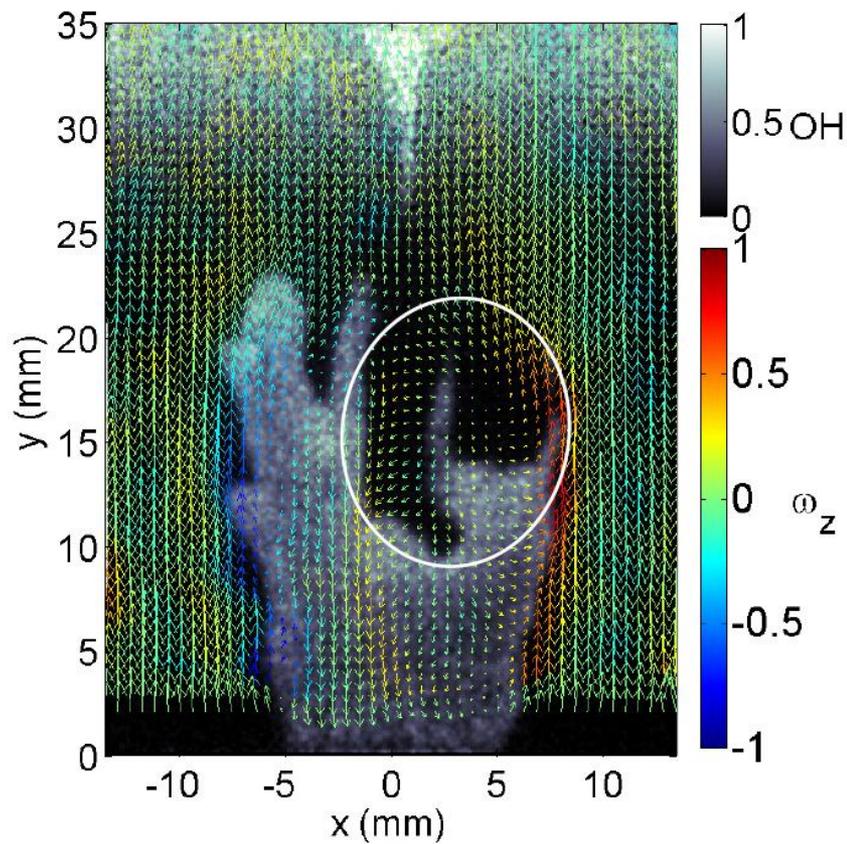
Flame images obtained by reversing the Mie scattering images obtained during the PIV experiments for the 10-mm-diameter disk-shaped bluff-body flame holder (arrows show the length scale  $\lambda = U_m/f$ ). (The values in black represent the ratio of the length of recirculation zone to  $\lambda$ ).

Mean flow and PLIF fields for  $U_m = 10\text{m/s}$   $f = 200\text{Hz}$   $L_{RZ_{\text{mean}}}/\lambda_{\text{mean}} = 0.4$

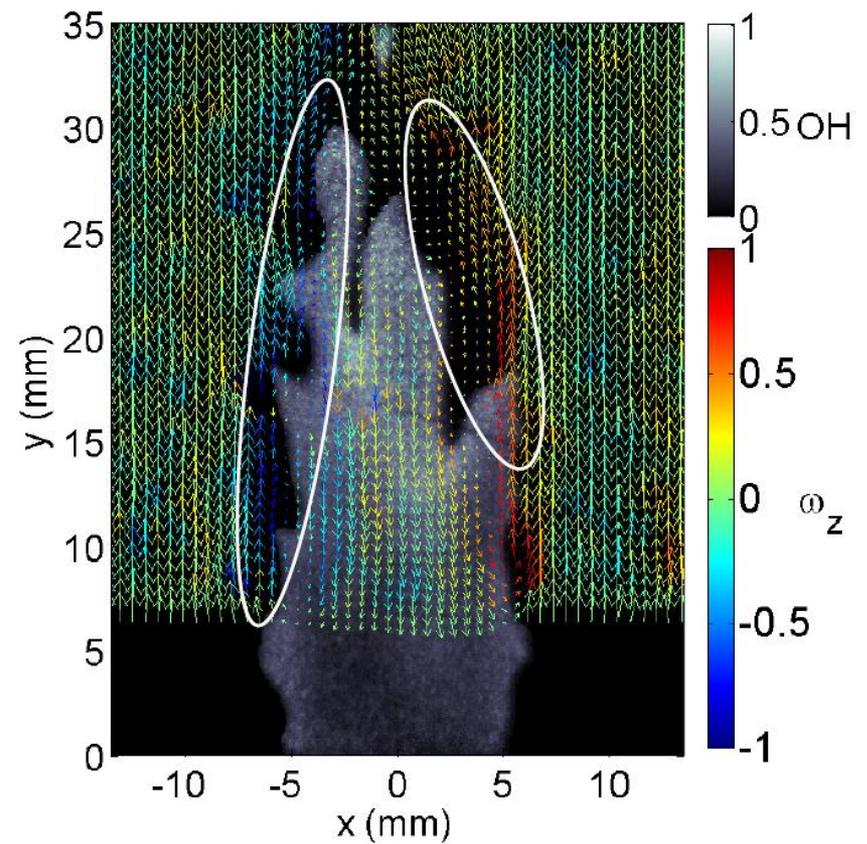


# Forced Blowoff : Forced Vortex Shedding

Forced Blowoff



Unforced Blowoff



# Blowoff in Swirl Stabilized Flames (Ga.Tech)

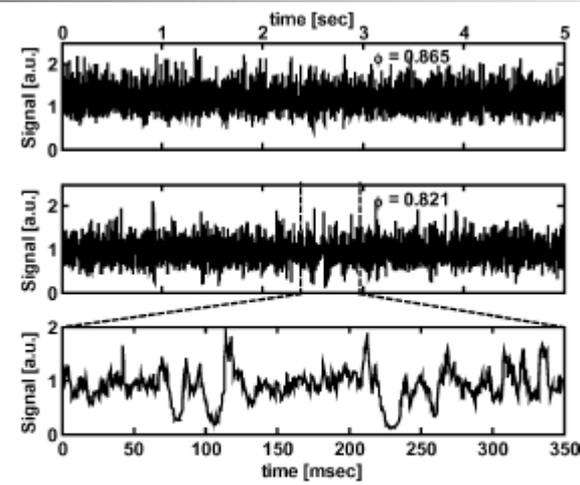
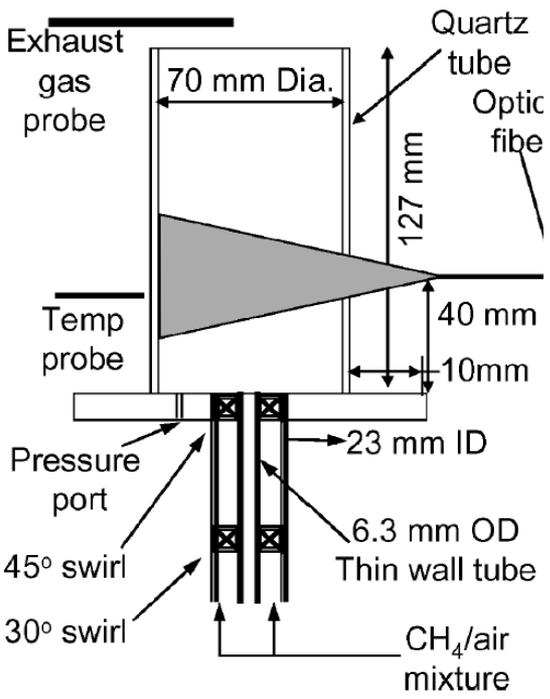
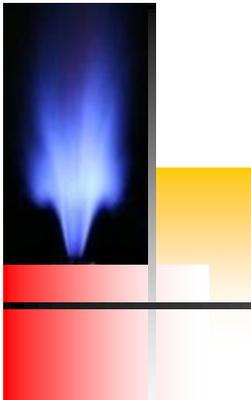


Fig. 2 Time-series data of OH chemiluminescence signal for equivalence ratio  $\phi = 0.865$  and  $0.821$  ( $\phi_{LBO} = 0.802$ ). The expanded time series for the last case is also shown.

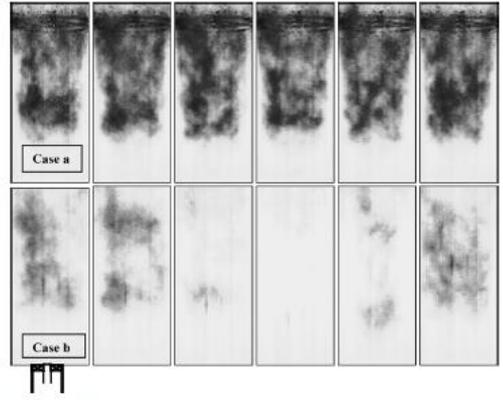


Fig. 3 High-speed visualization images (inverted grayscale): case a, equivalence ratio  $\phi = 0.79$ , time between images 2 ms; and case b,  $\phi = 0.76$ , time between images 16 ms showing a nearly total loss of flame followed by reignition ( $\phi_{LBO} = 0.745$ ). The location of the combustor inlet is indicated in the first image of case b.

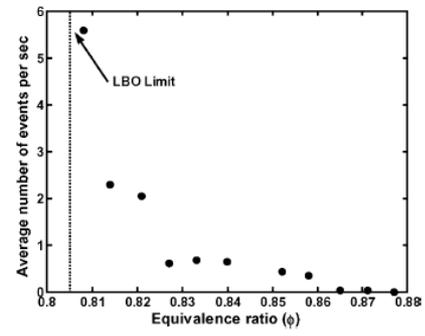
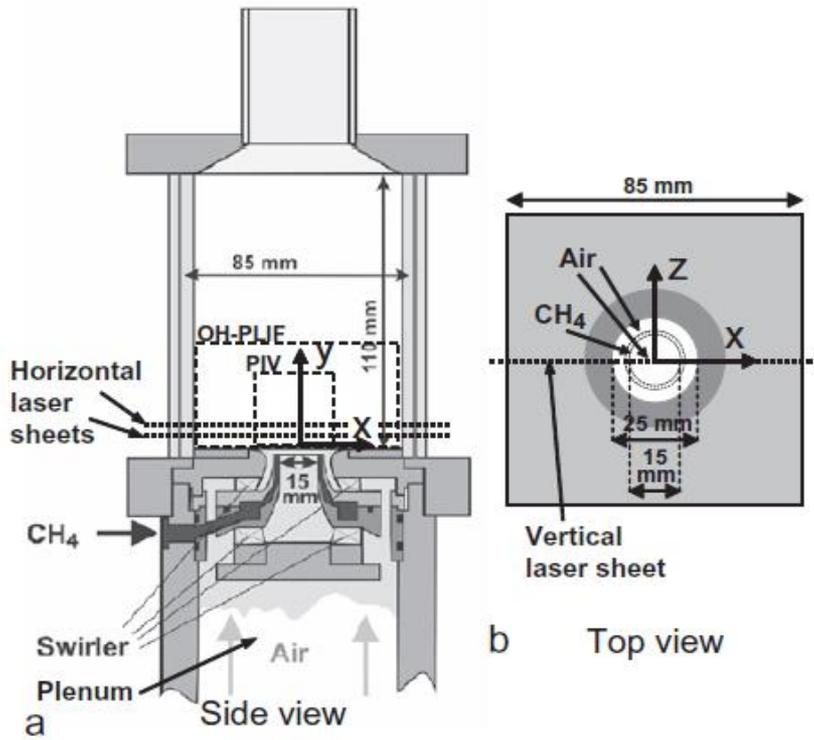
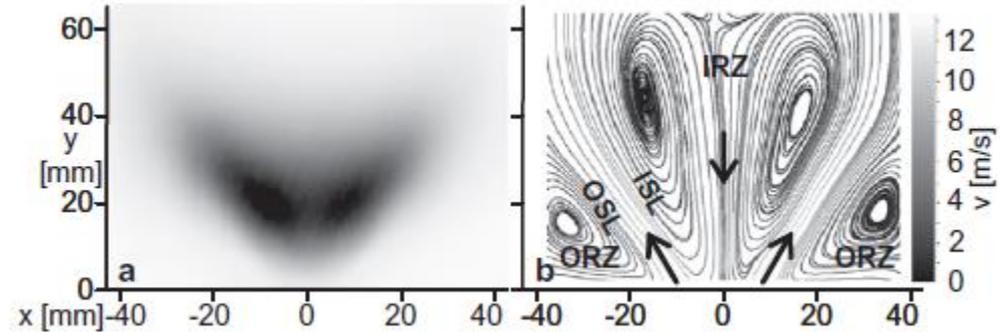


Fig. 5 Variation of average number of events per second as a function of equivalence ratio: ····, LBO limit for these conditions.

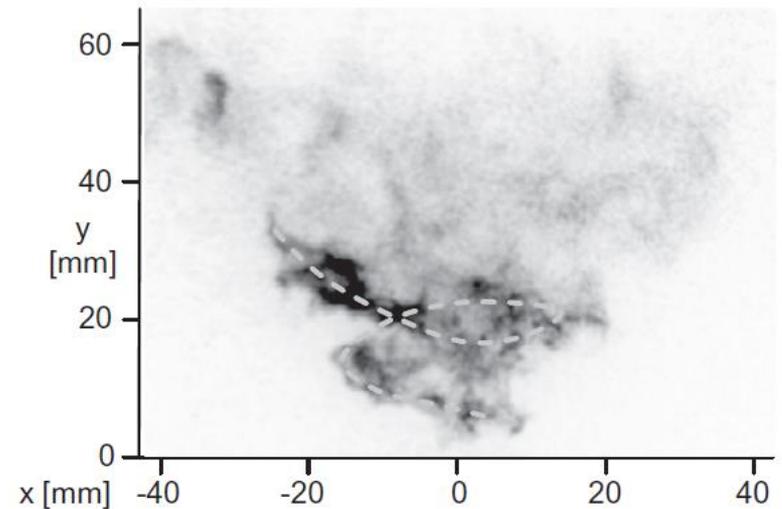
# Blowoff in Swirl Stabilized Flames (DLR)



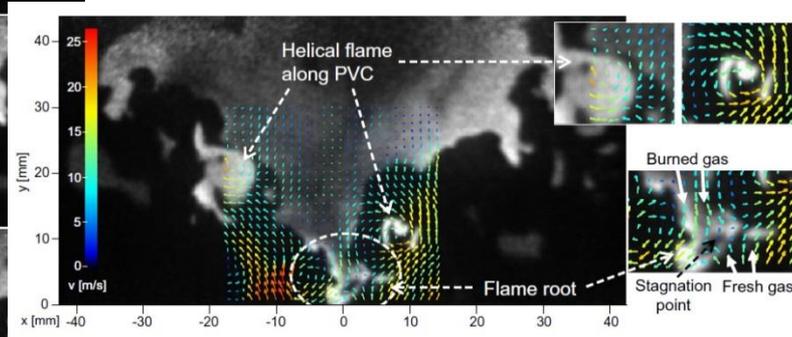
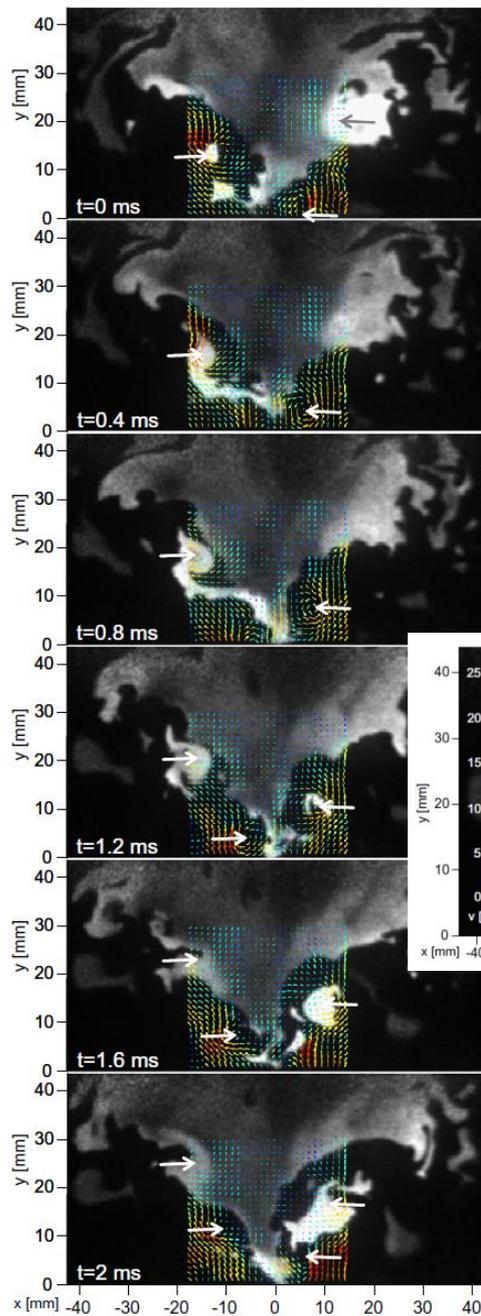
Experimental Setup



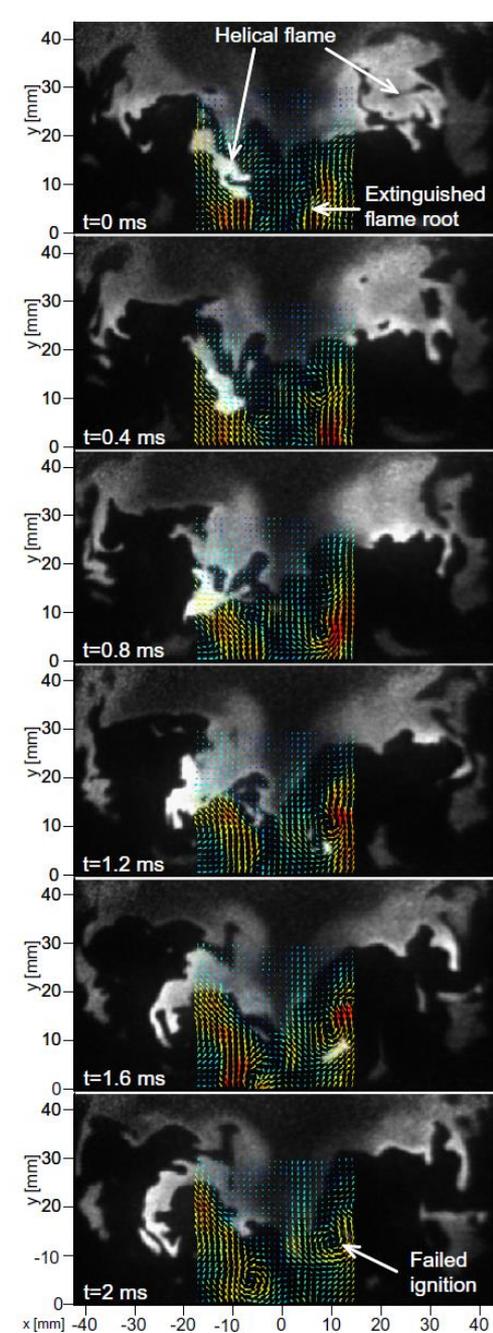
Time averaged OH\* and streamlines



# Near and Final Blowoff

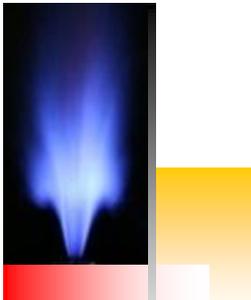


Enlarged views



Final blowoff

Consecutive images with PIV-PLIF near blowoff

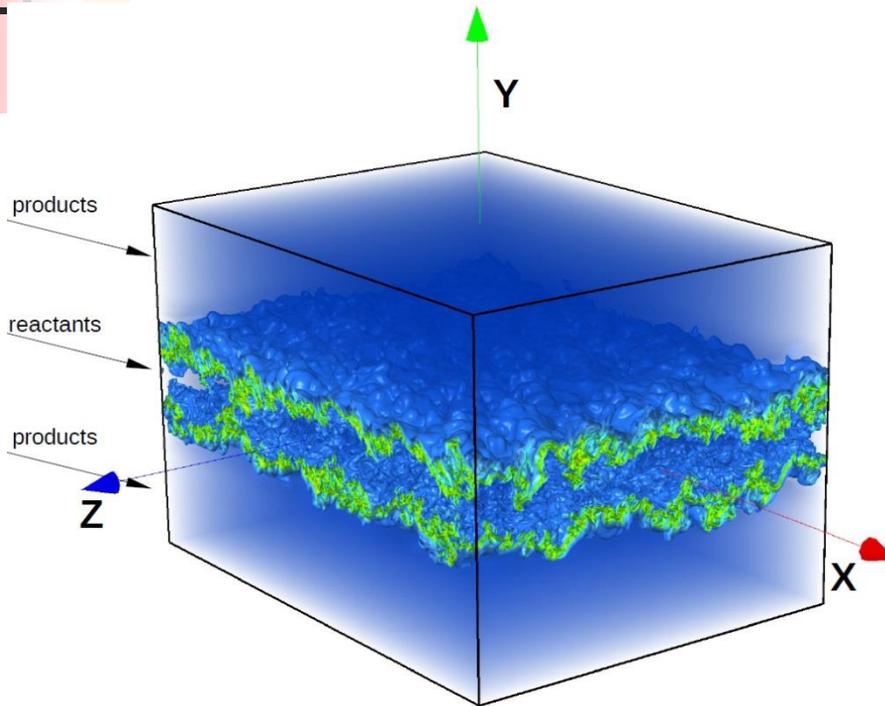
A small image in the top left corner showing a blue, swirling flame being extinguished, with a yellow and red gradient background behind it.

## Swirling flame blowoff

- Reaction occurs in helical zone along PVC (low SR); lower stagnation zone (high SR)
- This lower root flame region determines the rest of the state of the flame (in PVC), is inherently unstable.
- Finding is consistent with earlier work by Muruganandam and Seitzman who controlled blowoff by a pilot flow at the center.
- If the root remains extinguished for more than 2 ms (time scale of PVC) no relight is possible and flame blows off.

# DNS of H<sub>2</sub>-air flames

- DNS of temporally evolving planar premixed jet flame [1]
- Lean H<sub>2</sub>-air ( $\phi=0.7$ ) jet at  $Re = 10,000$ ,  $T_u = 700$  K



|     | <b>H</b><br>(mm) | $\Delta U$<br>(m/s) | <b>Da<sub>jet</sub></b> |
|-----|------------------|---------------------|-------------------------|
| Da- | 2.7              | 312.6               | 0.13                    |
| Da+ | 5.4              | 156.3               | 0.54                    |

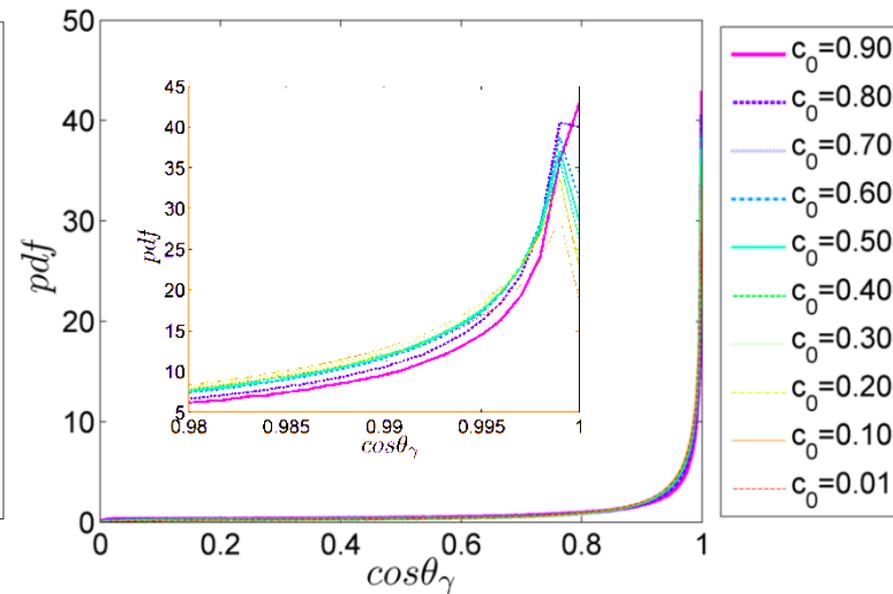
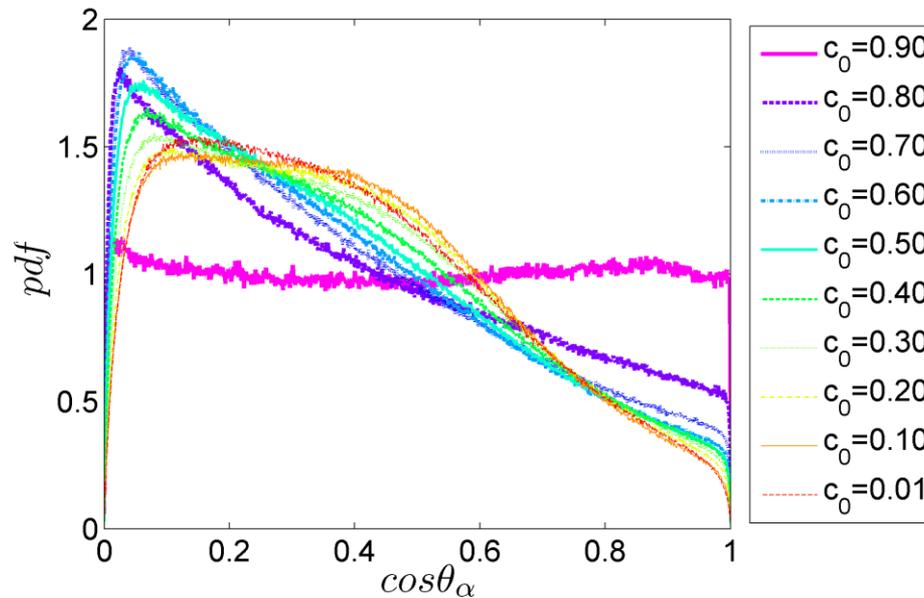
- DNS code S3D [2]; Mechanism of Li *et al.*, [3] (9 species, 19 reactions).
- Simulations performed on 120,000 cores of Jaguar Cray XT5 at ORNL by J. H. Chen group at Sandia.

[1] Hawkes et al. 2009, Comb. Flame. 159-2690.

[2] Chen et al. 2009, Comp. Sci. Disc. 2-015001.

[3] Li et al. 2004, Int. J. Chem. Kin., 80.

# Alignment statistics between surface normal and principal component of strain rate tensor



In both cases the flame normal is almost perfectly aligned with the most compressive strain and this alignment improves with increasing  $c_0$



Thanks and Questions